



## User manual for teh PWR-PLASIM model

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by  
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## Abstract

The report presents the implementation of the PWR power plant model PWR-PLASIM described in Risø Report No. 318. It should serve as a users guide for both the operator, who runs the model, and the experienced simulation engineer, who modifies the input data or details in the model.

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# 1. GENERAL INFORMATION

This report presents the implementation of the PWR power station model described in Ref. 1. Numerical data for the Westinghouse Surry-1 power station have been used as a test example, as most of the data needed for the model could be found in the available information, Refs. 2 and 3. For the turbine-reheater, however, some additional data had to be estimated from descriptions of the Obrigheim and Oyster Creek turbines.

The presentation follows the layout in Ref. 1. The same division in chapters and numbering of equations are used. The intention is that the report should serve as a handbook for the experienced simulation engineer, and facilitate the insertion of new data sets or modifications for special investigations. The present chapter, together with appendices A to F, should be sufficient to run the model, when it is prepared for a given station. Some information fundamental both for operation and modification of the model is given here, while the appendices contain all program listings, analog diagrams, potentiometer lists and other related information.

The analog part of the model is stored on a patchpanel according to the diagrams in the appendices. Any modification introduced later on must be thoroughly documented. The programs in the version given in the appendices are stored on the DEC-tape named "PWR DEC. 74" together with the system libraries as used at the time of storage. No modifications whatsoever may be introduced into this DEC-tape; it shall at all times serve as a basic model until and if a new, fully documented, version is available. The program system contains the following files for the station model:

- PWR.SB : The main PDP8 code section
- PWR1.SB: Neutron kinetic calculation in FPP-code
- PWR2.SB: Calculations for the primary circulation, the steam generator, the turbine and the reheater in FPP-code
- PWR3.SB: FPP-code sections for IC input and logging of main variables and the steam generator
- PWR.IC : A set of IC-data for fuel, moderator, steam generator, turbine and reheater
- PWR.ST and PWR.SP

PWR.SP : Potentiometer data for the analog model.

PWR.ST : A set of static data for the reactor calculated by a static program.

PWR.SV : The binary version of PWR.8B, PWR1.8B, PWR2.8B and PWR3.8B

The DEC-tape further contains the files for the independent models of separate components:

P1.8B : The pressuriser simulation program.

P2.FT : The ten-section fuel model.

P3.FT : The steam generator model.

P3100.IC: A set of IC values for the steam generator at full load.

Appendix K gives a list of the contents of the DEC-tape.

The programs with the file name extension FT are written in Fortran IV, while those with extension 8B are written in a macro language called HYBAL with macro instructions and subroutines developed just for hybrid simulation on the EAI680-PDP8-FPP12 machine.

The following section gives some basic operating instructions and explains the computation sequence.

After installing the patchpanel on the analog machine, the potentiometers must be adjusted by the Fortran program SETAN according to the potentiometer list PWR.SP. The Q-potentiometers must be adjusted manually.

The simulation program PWR.SV can then be started. It prints a message on the DEC-writer to remind the operator of the adjustments of limiters and pulse generators listed in appendix F, and of the switch 0 (see below).

The computation must be started on a set of either IC-data for the whole station, or static data for the reactor alone. The IC-data are inserted automatically from the disc file PWR.IC during the analog IC period, when the logic connection to DI(11) is in function. The insertion is announced by a message containing the regulating rod position and the electrical load. The two potentiometers, Q14 and Q29, must be adjusted accordingly. The computations start bumpless, when the analog computer is set at OPERATE. The PDP8 is synchronized via pulses over DI(0) at a rate of 10 per sec. The same pulses synchronize the display, where one or more variables along the reactor axis may be selected. The time

representing the length of the space axis may be adjusted in the range 10-25 mS by MM 0.

For a new set of reactor conditions without a full set of IC-data a set of static data must be generated by the static program described in Ref. 4. The data must be stored in a disc file PWR.ST before they can be used in PWR.SV. They are inserted into PWR.SV by printing the number "2" on the DEC-writer with the analog machine in PC mode. The insertion is announced on the DEC-writer by a message containing the regulating rod position and the approximate power level. The two potentiometers, Q14 and Q29, must be adjusted accordingly. When the computation are started via the analog IC-mode, the connection to DI(11) must be withdrawn to avoid insertion of IC-data from file PWR.IC. The computations do not start bumpless, as it is most likely that the IC-data in the potentiometer list do not fit the new reactor condition exactly, but within a few minutes a new stationary state with the required value of reactor load and steam pressure may be found by adjustments of the regulating rod, the boron acid concentration and the electrical power load. Fast transients in the first few seconds will most likely overload the output channels from the pressuriser model. This can be avoided and the transient time decreased by pressing switch 0 before the start. The switch is connected to DI(2) which controls the operation of the pressuriser, taking it out of action for switch 0 equal to "1". The pressuriser is reconnected, when the transients have died out. The new state may be stored on a disc file PWR.IC by typing "1" on the DEC-writer with the analog computer in HOLD mode. For later use of the file, the IC-data in the potentiometer list must be corrected manually by reading the integrator outputs, and both new files must be stored as a set on DEC-tape. The main variables may be listed on the DEC-writer for documentation by typing "3" on the DEC-writer with the analog machine in HOLD mode.

The computations are controlled by the PDP 8 code program in file PWR.8B synchronized by pulses on DI(0) conditioned by the OPERATE state. A pulse starts the calculation sequence with the routine HYDRAL, which controls the hybrid calculations for the reactor core heat transfer. This follows HYDRAL, which calculates for PFP calculations of the primary loop and the steam generator parameters and the secondary loop. HYDRAL2 initiates these calculations.

FPP2 and TURB, and calculates the sum of the reactor thermal power for later use. Next follows, in HYDRA3, the calculation of the boron acid distribution in the primary loop in 12-bit integer arithmetic. HYDRA4 reads the regulating rod position and calculates the rod density in the core sections ready for use in the neutron kinetics routine. The final PDP8-routine is HYDRA5, which is started when the FPP unit finishes the calculations initiated in HYDRA2. HYDRA5 starts calculating the neutron flux distribution in the FPP-routine FPP1, performs all the adjustments of analog outputs and the MDACs, and finally starts the FPP3 routine with calculation of the delayed neutron concentrations, when the neutron kinetic routine is finished. The FPP3 routine is followed by the PROP routine with the calculations for the pressuriser. From HYDRA5 PDP8 goes back to the waiting loop, while the FPP unit continues the calculations just started, which normally last some few milliseconds into the next time interval.

The calculations may run into error conditions which prevent continuation. In these cases a message is typed on the DEC-writer and the program stopped with a jump to monitor. A list of error messages is given in Appendix F.

The waiting loop in the PDP8 code contains a test of the DEC-writer request. If a request is detected, the character will be printed and action taken according to the following list.

- 0: Go to the FPP input-output test routine belonging to the HYBAL language.
- 1: Transfer a set of IC-data for the present steady state condition to the disc file PWR.IC.
- 2: Transfer a set of reactor static data from disc file PWR.ST to the data areas in the core for the active PWR.SV program.
- 3: Type a list with main variables and parameters on the DEC-writer.

Other characters: no action.

Analog simulation requires amplitude scaling. The variable range on the analog machine is defined as  $\pm 1$  corresponding to  $\pm 10V$ . A variable  $X$  with the variation  $\pm X_{max}$  must be used with a scale factor  $SF X = 1/X_{max}$ . A variable with a scale factor is written in square brackets, e.g.  $[0.02 T_c]$ . The same convention is used for integer variables in the PDP8 where  $\pm 1$  corresponds to the

integer  $\pm 2048$ . In a single case another type of scale factor is needed for integer arithmetic; the meaning is given by the equation:

$$X \text{ in machine integer units} = ((SF X) \times X) .$$

The scale factor is chosen so the maximum value of  $X$  corresponds to the integer 4096 for positive variables and  $\pm 2048$  for dual signed variables. The analog input and output units work with dual signed integers, while the MDACs only use positive integers.

The interface units will often be referred to by abbreviations as follows:

AI: analog input channels  
 AO: analog output channels  
 DI: digital input  
 DO: digital output  
 MDAC: multiplying digital to analog converters

Other abbreviations are:

A: analog amplifier  
 P and Q: potentiometers  
 DFG: diode function generators  
 NM: Monostable timers given adjustable pulse length

## 2. NEUTRON KINETICS

### Geometrical data

Number of core sections: 14

Length of core : 365 cm

$A_x = 365/14 = 26.07 \text{ cm}$

$V_f = 1.784 \text{ m}^3$

# Physical data

The kinetic parameters  $D$ ,  $\Sigma_a$  and  $\nu I_f$  have been calculated by static programs as second degree polynomials in the 5 variables:  $T_u$ ,  $T_c$ ,  $\rho_m$ ,  $C_b$  and CR. The control rod density CR has been normalized as a quantity between 0 and 1. The other 4 variables are used with suppressed zero points. The following values are used:

$T_u$  : 735 °C  
 $T_c$  : 298 °C  
 $\rho_m$  : 0.7296 g/cm<sup>3</sup>  
 $C_b$  : 1500 ppm

The general formulae are:

$$a_1 \Delta T_c^2 + a_2 \Delta T_c + a_3 \Delta \rho_m^2 + a_4 \Delta \rho_m + a_5 \Delta C_b^2 + a_6 \Delta C_b + a_7 CR + a_8 \Delta T_u^2 + a_9 \Delta T_u + a_{10}$$

For the reflector sections,  $a_8$  and  $a_9$  are omitted.

In the diffusion equation  $\Sigma_a$  and  $\nu I_f$  are always used together in the common expression  $(1-\beta)\nu I_f - \Sigma_a$ , so it is an advantage to use a polynomial for  $(\nu I_f - \Sigma_a)$ , completely eliminating the need for  $\Sigma_a$  alone.  $\nu I_f$  alone is needed for calculation of the delayed neutrons and the thermal power, but here a less accurate calculation is possible. The variation of  $\nu I_f$  with  $T_u$  and  $T_c$  is less than 1% in the temperature range of interest, so it is completely neglected. The variation with  $C_b$  is nearly linear below 2000 ppm, which is the upper limit, so only a first order term for  $C_b$  is used. The terms for  $\rho_m$  and CR are used unchanged. All the data for the kinetic polynomials are given in table 2.1.

The delayed neutrons are represented by 3 groups with the following data:

$\beta_1 = 992E-6$	$\lambda_1 = 1.82$	$s^{-1}$
$\beta_2 = 3840E-6$	$\lambda_2 = 0.249$	$s^{-1}$
$\beta_3 = 1616E-6$	$\lambda_3 = 0.0288$	$s^{-1}$
$\beta = 6448E-6$		

Data for conversion of neutron flux  $\phi$  to thermal power N:

$A = 0.3E-10$  J/fission  
 $\nu = 2.43$  neutrons/fission

Insertion in eq. (2.9) gives:

$$N = (2.18E-11)\nu I_f \phi \quad \text{MW/section} \quad (2.9)$$

## 2.1. Digital routines

The kinetic equations are solved by the digital routines FPP1 and FPP3 in file PWR1.8B, appendix A.

The first file page contains all the numerical data and variables.

The second file page contains the routine for calculation of the kinetic parameters and the coefficients in the matrix equation (2.8). The integer variables  $T_u$ ,  $T_c$ ,  $\rho_m$ ,  $C_b$  and CR are transferred from the arrays A0-A15 in the PDP8 code section in file PWR.8B and converted to floating point form.

The third file page contains the routine for solution of the equation (2.8), calculation of  $\nu I_f \phi$  for the next routine and of the thermal power N, which is converted to integer form and stored in array N, with a scale factor 1/500. By the conversion overflow is possible during power transients. A test for overflow is carried out for fuel sections 3-10 and announced by a TRAP6 message no. 0-7.

The fourth file page contains the routine FPP3 for calculation of the delayed neutrons. It is not coupled to the preceding routine FPP1, but is activated independently.

The regulating rod position is an independent control variable, which is inserted via AI7 through the PDP8 routine HYDRA in file PWR.8B. The rod density in each section is represented by a number between 0 and -2048 inclusive.

Numerical data in file PWR1.8B

Array KD: coefficients  $a_1$ - $a_{10}$  for D

" KSFA: " " "  $(vE_f - E_a)$  in the core  
 " KSF: " " "  $vE_f$   
 " KD0: "  $a_1$ - $a_8$  " D  
 " KSA0: " " "  $E_a$  ) in the reflector

$$DX2 = \Delta x^2 = 679.645$$

$$F3DX = 3\Delta x = 78.21$$

$$DXR = 1/\Delta x = 0.038358$$

$$BETA = \beta = 6.448E-3$$

NPTU = "Analog zeropoint" - "Digital zeropoint" for  $T_u$

$$= 800 - 735 = 65$$

NPTC = do. for  $T_c$

$$= 300 - 298 = 2$$

NPRO = do. for  $\rho_m$

$$= 0.5 - 0.7296 = -0.2296$$

NPBO = do. for  $C_b$

$$= 0 - 1500 = -1500$$

$$SFTU = -1/(SF T_u \times 2048) = -500/2048 = -2.4414E-1$$

$$SFTC = 1/(SF T_c \times 2048) = 50/2048 = 2.4414E-2$$

$$SRRO = 1/(SF \rho_m \times 2048) = 0.5/2048 = 2.4414E-4$$

$$SFBO = 2000/4096 = 4.8828E-1$$

SFCR = -(weighting factor for regulating rod/2048)

$$= \text{e.g. } -0.25/2048 = -1.2207E-4$$

(updated by input of static data or IC data)

$$SFN = 2.18E-11 \times 4096 \times SF N = 2.18E-11 \times 4096/500 = 1.7859E-10$$

(equation (2.9))

$$LM1 = \lambda_1 = 1.82$$

$$LM2 = \lambda_2 = 0.249$$

$$LM3 = \lambda_3 = 0.0288$$

$$CN1K2 = (2 - \lambda_1 \Delta t)/(2 + \lambda_1 \Delta t) = 0.833181$$

$$CN1K1 = 2\beta_1 \Delta t/(2 - \lambda_1 \Delta t) = 1.091309E-4$$

$$CN2K2 = (2 - \lambda_2 \Delta t)/(2 + \lambda_2 \Delta t) = 0.975406$$

$$CN2K1 = 2\beta_2 \Delta t/(2 - \lambda_2 \Delta t) = 3.888411E-4$$

$$CN3K2 = (2 - \lambda_3 \Delta t)/(2 + \lambda_3 \Delta t) = 0.997124$$

$$CN3K1 = 2\beta_3 \Delta t/(2 - \lambda_3 \Delta t) = 1.618330E-4$$

Arrays for parameters and variables

CCR: Fixed control rod density.

CJI: Elements below the diagonal in {C} with first position empty.

CJJ: Elements in the diagonal in {C}.

CJK: Elements above the diagonal in {C} with last position empty.

PHI:  $\phi$

FNP:  $vE_f \phi$

NYSF:  $vE_f$

SAZE: Fixed contribution to  $I_a$  from xenon poisoning calculated in  
and transferred from the static program.

SLCN:  $I_{aCn}$

CN1:  $C_1$

CN2:  $C_2$

CN3:  $C_3$



	D	$\Sigma_a$	$v\Sigma_f$	$v\Sigma_f - \Sigma_a$	$v\Sigma_f$ simplified
a <sub>1</sub>	1.275E-6	6.925E-8	1.0775E-7	3.85E-8	-
a <sub>2</sub>	-4.700E-5	-1.485E-6	-2.150E-6	-6.65E-7	-
a <sub>3</sub>	6.4587	-1.3714E-1	-1.459E-1	-8.76E-3	-1.459E-1
a <sub>4</sub>	-4.7908E-1	1.2717E-2	1.3522E-2	8.05E-4	1.3522E-2
a <sub>5</sub>	1.400E-9	7.800E-11	3.016E-10	2.236E-10	-
a <sub>6</sub>	1.100E-5	3.402E-7	-1.724E-6	-2.0642E-6	-1.9E-6
a <sub>7</sub>	6.6E-3	2.4E-4	-6.4E-4	-8.8E-4	-6.4E-4
a <sub>8</sub>	2.7665E-9	1.7956E-10	4.8171E-10	3.0215E-10	-
a <sub>9</sub>	4.5499E-6	2.1279E-7	-3.9407E-7	-6.0686E-7	-
a <sub>10</sub>	1.2033	2.55E-2	2.6391E-2	8.91E-4	2.6391E-2

Table 2.1

Coefficients for polynomial calculation of kinetic parameters.

## 3. THE FUEL MODEL

Geometrical core data

$\Delta x = 26.07$  cm  
 $M_u = 204 \times 157 = 32028$   
 $r_u = 0.4655$  cm  
 $\Delta r_g = 0.0080$  cm  
 $\Delta r_{ca} = 0.0620$  cm  
 $r_{ca} = 0.5355$  cm  
 $H_{ca} = 3.170$  cm<sup>2</sup>/cm  
 $O_{ca} = 280.9$  m<sup>2</sup>/section  
 $D_{ec} = 0.01435$  m  
 $A_c = 3.88$  m<sup>2</sup>  
 $V_c = 1.012$  m<sup>3</sup>/section

Physical fuel data

$k_g = 4.0$  W/cm<sup>2</sup>C  
 $\lambda_{ca} = 0.15$  "  
 $Z_{ca} = \Delta r_{ca} / (H_{ca} \lambda_{ca}) = 0.1304$  cm<sup>2</sup>/W  
 $Z_{gca} = Z_{ca} + 1/k_g = 0.3804$  "  
 $Z_{gca}$  per section = 0.4556 °C/MW  
 $\rho_{ca} = 6.5$  g/cm<sup>3</sup>  
 $c_{ca} = 0.31$  J/g°C  
 $\rho_u = 10.0$  g/cm<sup>3</sup>  
 $c_u = 0.32$  J/g°C  
 $C_{ca} = 0.3307$  MJ/°C per section  
 $C_u = 1.819$  " " "  
 $\lambda_u = (4.788E-13)T^3 + 38.24/(T + 129.4)$  W/cm<sup>2</sup>C (T in °K)

3.1. The ten-shell section fuel model

The model has been implemented in a Fortran program suitable for calculation of transients for variation in either the heat production, N, or the coolant temperature, T<sub>c</sub>. The program works in real time synchronized from the analog computer. It receives the input variables N and T<sub>c</sub> from analog inputs, and delivers the output via analog output channels and the DEC-writer. The program and the analog diagram are given in appendix G with implementation for steps in N and T<sub>c</sub>.

The program is divided into sections numbers 1 to 9. Section 3 contains all the geometrical and physical data in DATA statements. Section 4 calculates some fixed parameters and resets digital inputs and outputs. Section 5 contains a waiting loop for the timing impulse via DI6; when the impulse arrives the calculation starts by reading the input variables which are:

AI0: (N/500)

AI1: ((T<sub>ci</sub>-200)/50).

The time step is 0.1 sec. so 10 pulses are used for the calculation. Sections 6 and 7 calculate the matrix equation (3.1.4) and solve for the

some variables for analog outputs and performs the output function. The output variables with scale factors and zeropoints are:

$$A00: ((T(1) - 1500)/1000)$$

$$A01: ((T_{\text{mean}} - 1000)/500)$$

$$A02: ((T(10) - 500)/250)$$

$$A03: ((T_{\text{ug}} - 500)/200)$$

$$A04: ((T_{\text{ca}} - 300)/100)$$

$$A05: ((Q_c - 250)/250)$$

Output printout can also be obtained at the DEC-writer by a signal at DI7. For every sampling time the program asks if DI7 is set and gives a printout if it is true. A periodic printout can be obtained with the counter circuit shown in the analog diagram; the period can be selected by the preset time thumb wheels. The variables in the printout are the ten  $T_u$  temperatures on the first line, and the following variables on the second line:  $T_u(\text{mean})$ ,  $T_{\text{ug}}$ ,  $T_{\text{ca}}$  and  $Q_c$ .

### 3.2. The two-point fuel model

The equations (3.2.1) and (3.2.2) are given here with numerical values, but all other details are given in the next chapter, as all the core heat transfer equations are used in one hybrid routine.

$$\dot{T}_u = 0.5498(N - k_f(T_u - T_{\text{ca}}))$$

$$\dot{T}_{\text{ca}} = 3.0239(k_f(T_u - T_{\text{ca}}) - Q_c)$$

$$\frac{1}{k_f} = Z_{\text{ugca}} = \frac{4.65E-6}{2u} + 0.4556$$

$$T_{\text{ug}} = T_{\text{ca}} + 0.4556 k_f (T_u - T_{\text{ca}}) \quad \left. \begin{array}{l} \dot{T}_u \\ \dot{T}_{\text{ca}} \\ \frac{1}{k_f} \end{array} \right\} (3.2.1)$$

$$\lambda_u = F_{\lambda}(\frac{1}{2}(T_u - T_{\text{ug}}))$$

$$Q_u = k_f(T_u - T_{\text{ca}})$$

$$T_u(n+1) = T_u(n) + \Delta_t T_u$$

$$\Delta_t T_u = 0.05498(N(n) - k_f(T_u(n+\frac{1}{2}) - T_{\text{ca}}(n+\frac{1}{2})))$$

$$T_{\text{ca}}(n+1) = T_{\text{ca}}(n) + \Delta_t T_{\text{ca}} \quad \left. \begin{array}{l} \Delta_t T_u \\ T_{\text{ca}}(n+1) \end{array} \right\} (3.2.2)$$

$$\Delta_t T_{\text{ca}} = 0.3024(k_f(T_u(n+\frac{1}{2}) - T_{\text{ca}}(n+\frac{1}{2})) - Q_c(n+\frac{1}{2}))$$

The coefficient  $K_u = 4.65E-6$  is selected so  $T_u$  obtains the same static values as the  $T_u$  mean value for the 10-shell section at a section load of 250 MW.

## 4. THE PRIMARY CIRCUIT WITH HEAT TRANSPORT AND BORON ACID CONCENTRATION

### 4.1. Heat transfer in core

All geometrical data are included in the list in chapter 3.

Only some few physical parameters, which are nearly constant over the working range or are of minor importance, are taken as constants. These are:

$$h_c(T) = 0.92 \text{ KJ/kg}^\circ\text{C} (\text{kg/m s})^{0.2} \text{ for eq. (4.5)}$$

$$h_{fg} \rho_{gs} = 97.1 \text{ MJ/m}^3 \quad " \quad (4.9)$$

$$\rho_f = 725 \text{ kg/m}^3 \quad " \quad (4.9)$$

$$\rho_f - \rho_{gs} = 630 \text{ kg/m}^3 \quad " \quad (4.10)$$

Other parameters are taken as temperature-dependent functions.

The equations with numerical values are listed below. Eq. (4.6) is simplified by using  $\exp(p_p/43.4)$  as a constant. It is justified by small variations in the primary pressure  $p_p$  and by the quadratic term  $(T_{\text{ca}} - T_{\text{ps}})^2$ , which makes  $T_{\text{ca}}$  insensitive to variations in the coefficient.

$$T_c(j, n+1) = T_c(j-1, n+1) + \frac{1}{W_c} \left( \frac{Q_c(j)}{C_p} - 10.12 \rho_f \Delta_t T_c(j, n+1) \right)$$

$$\Delta_t T_c(j, n+1) = T_c(j, n+1) - T_c(j, n) \quad \left. \begin{array}{l} T_c(j, n+1) \\ \Delta_t T_c(j, n+1) \end{array} \right\} (4.7)$$

$$Q_{c1} = 4.695E-3 W_c^{0.6} (T_{\text{ca}} - T_c)$$

$$Q_{c2} = 17.57 (T_{\text{ca}} - T_{\text{ps}})^2$$

$$Q_b = Q_c \cdot F_v(T_{\text{ps}} - T_c)$$

$$Q_t = Q_c - Q_b$$

$$a(j, n+1) = a(j-1, n+1) + \frac{Q_c(j)}{W_c}$$

$$a_c(j, n+1) = a_c(j, n) + \frac{Q_c(j)}{W_c}$$

$$p_m = p_g = 520 \text{ atm}$$

These equations are solved together with the fuel equations in one hybrid routine, where the calculations are done by analog components with the digital machine as coordinator and store medium. The same circuits are used for all the core sections on a serial basis with parallel analog calculations. This gives a computing time of about 1 ms per section. The input to the routine is the thermal power  $N$ , the coolant inlet temperature  $T_{ci}$ , with the coolant flow rate as a variable input parameter. The output variables are temperature profiles for the fuel, the casing and the water together with void and water density profiles, all stored as 12-bit integers in the digital machine.

The latest investigations of the void production carried out by the static program show that the dynamic void calculations are inadequate, but also without importance in the working range for the dynamic model. The void mechanism should be further studied and the model improved, or the void representation should be completely omitted. The data for the function  $f_v$  given in appendix B are consequently arbitrary and not based on static calculations.

The analog diagram is given in appendix B together with scaled equations, DFG tables and potentiometer lists. Suppressed zero-points are used in order to improve the signal resolution in the AD/DA conversion. The zeropoints are:

$T_u$  : 800 °C  
 $T_{ca}$  : 300 °C  
 $T_c$  : 300 °C  
 $\rho_m$  : 500 kg/m<sup>3</sup>.

The scale factors and the corresponding working ranges are:

SF  $N$  = 1/500 Range: 0-500 MW/section  
 SF  $Q_u$ , SF  $Q_c$  = SF  $N$   
 SF  $T_u$  = 1/500 Range: 800 ± 500 °C  
 SF  $T_{ca}$  = 1/100 Range: 300 ± 100 °C  
 SF  $T_c$  = 1/50 " : 300 ± 50 °C  
 SF  $\alpha$  = 10 " : 0-0.1  
 SF  $\rho_m$  = 1/500 : 500 ± 500 kg/m<sup>3</sup>

SF  $c_p$  = 100 Range: 0-0.010 MJ/kg °C  
 SF  $(1/\lambda)_u$  = 2 E-6 " for  $\lambda$ : (2-5)E-6 MW/m °C  
 SF  $W_c$  = 1/15000 " : 5000-15000 kg/s

Other scale factors for intermediate variables may be found in the list of scaled equations.

The digital routine, HYDRAL, that controls the calculations is found in file PWR.8B, appendix A. The routine uses 3 internal subroutines: HIC, OPDA and TRVENT, and one library subroutine, DIVI. HYDRAL links directly to the next routine HYDRA2, which is discussed in section 4.2.

The computing sequence for a core section consists of 3 steps. First, the old outlet values are set on analog output channels and MDACs, while track-store amplifiers fetch the new inlet values to the section in question. Second, the computing circuit is switched to the computing mode to find the new set of outlet values; during the amplifier transients the digital machine is used to update the stored values for the previous section. Third, the changes for the new outlet values are read into the digital machine, and the computing circuits are switched to store and track mode. The first core section requires a special subroutine, HIC, for initialization. At the end the hybrid routine is used one extra time to convert the heat stored in steam to an increased water temperature.

The computation is controlled via the digital outputs DO(0' - DO(3) and the digital input DI(1), as shown in the diagram for the logic units. The "ic" signal is used to insert the inlet variables  $T_{ci}$  and  $\alpha(0) = 0$ ; "co" sets the track-store units in compute mode; the "ho" impulse shifts the section outlet value on one track-store amplifier to the inlet value on the other track-store amplifier. The "rs" signal is used to shift between the analog signals  $(Q_c - Q_b)$  and  $IQ_b$  sent out from PDP8 for the last section. The two pulses  $t_1$  and  $t_2$  can be used to control track-store amplifiers to sample and hold any signal for a selected section. The selection is done with the preset knobs for the constant SCDB and SCPL.

Some scale factor dependent numbers are distributed among the routines. These are all parameters for JMS DIVI:

# HYDRA1:

HL + 21 lines:  $(SF Q_k)/(SF EQ_k) = 10 = 12_8$   
 + 9 " :  $(SF A_t T_c)/(SF T_c) = 50/10 = 5$

# OPDA:

line 11:  $(SF A_t T_u)/(SF T_u) = 500/25 = 20 = 2^4_8$   
 + 5 lines:  $(SF A_t T_{ca})/(SF T_{ca}) = 100/25 = 4$   
 + 5 lines:  $(SF A_t T_c)/(SF T_c) = 50/10 = 5$   
 + 10 lines:  $(SF A_a)/(2 \times SF a) = 100/20 = 5$   
 + 11 lines:  $(SF Q_k)/(SF EQ_k) = 500/50 = 10 = 12_8$

The variables  $T_u$ ,  $T_{ca}$ ,  $T_c$ ,  $a$  and  $\rho$  are stored in the arrays A0-A15 as the first 5 elements. Element no. 6 is used for boron acid concentration, no. 7 for regulating rod density and no. 8 contains an index pointer with the array numbers from 0 to 15. The arrays are found in the last file page in file PWR.8B.

The communication between the two machines goes through the following units:

AI0 :  $(Q_b/50)$   
 AI1 :  $-(A_t T_u/25)$   
 AI2 :  $(A_t T_{ca}/25)$   
 AI3 :  $(A_t T_c/10)$   
 AI4 :  $(100 A_t a)$   
 AI5 :  $-(\rho_m - 500)/500$   
 AO1 :  $-(A_t T_u/500)_n$   
 AO2 :  $(A_t T_{ca}/100)_n$   
 AO3 :  $(A_t T_c/50)_n$   
 AO5 :  $(A_t T_c/50)_{inlet} \text{ or } (EQ_b/500)$   
 MDAC0 :  $(N/500)_n$   
 MDAC1 :  $(10 a)_n$

## 4.2. Heat transport in the primary circuit

The primary loop is divided into the following compartments:

Reactor upper plenum	46.00 m <sup>3</sup>
3 tube sections of	1.177 "
SG inlet chamber	4.57 "
2 SG U-tube sections of	10.45 "
SG outlet chamber	4.57 "
2 tube sections of	1.230 "
3 tube sections of	1.173 "
2 reactor downcomer sections of	6.625 "
reactor lower plenum	23.75 "

Only two physical quantities are needed and they are both used as constant values:  $\rho_f = 725 \text{ kg/m}^3$  and  $\frac{d\rho_f}{dT}$ , which is evaluated at 3 temperature levels: 285, 300 and 318 °C giving -1.80, -2.10, -2.60 kg/m<sup>3</sup>°C respectively.

The calculations are carried out in the digital routine FPP2 which is found in file PWR2.8B. The routine calculates in addition some steam generator parameters and links to the turbine power calculation. It is activated in the PDP8 routine HYDRA2 after insertion of input variables which are:

AI :  $(W_c/15000)$   
 AI14 :  $(W_p/5000)$   
 AI10 :  $(T_{po} - 300)/50$

The temperature calculations are made strictly according to the formulae (4.11) - (4.13). The sum term  $A_t T_c$  in (4.13) is calculated in the routine HYDRA1 and transferred to FPP2.

Conversion of the reactor lower plenum temperature to fixed form may result in overflow announced by the message TRAP 28. The reactor upper plenum temperature is sent out at MDAC 14 as  $(T_{up} - 250)/100$ .

The first file page in file PWR2.8B contains some numerical data which are:

Array VPL: The volumes as listed above

VC : 1 core section volume = 1.177

STWC :  $1/(2048 \times SF WC) = 1.177/2048$

STWP :  $1/(2048 \times SF WP) = 1.177/2048$

SFTIN :  $1/(2048 \times SF T) = 50/2048 = 0.0244141$   
 SFTUD :  $2048 \times SF T = 2048/50 = 40.96$   
 FDT :  $\Delta t = 0.1$   
 FROK :  $\rho_f = 725$   
 DRODTM :  $\frac{dp_f}{dt}$  at 300 °C = -2.10  
 DRODTH : " " 318 °C = -2.60  
 DRODTL : " " 285 °C = -1.80

The array TPL contains the temperature belonging to the volumes in VPL with an extra element for the outlet temperature  $T_{po}$  from the steam generator U-tubes.

#### 4.3. Boron acid distribution

2 tube sections of	1.173 m <sup>3</sup>
(the first is the insertion point for boron acid)	
2 reactor downcomer sections	6.625 "
Reactor lower plenum	23.75 "
4 reactor core sections of	3.54 "
Reactor upper plenum	46.00 "
3 tube sections of	1.177 "
SG inlet chamber	4.57 "
4 SG U-tube sections of	5.225 "
SG outlet chamber	4.57 "
2 tube sections of	1.230 "
1 tube section of	1.173 "

The calculations are carried out in the routine HYDRA3 in file PWR.8B. It follows directly after HYDRA2 mentioned in the previous section.

In order to save time for the floating point processor, fixed point arithmetic is used. The boron acid concentration is represented by 12-bit positive integers for the range 0-0.002

(0-2000 ppm) giving a scale factor  $SF C_b = 500$ . With  $SF W_b = 1$  eq. (4.14) scaled in machine units becomes:

$$\{500 C_b(o, n+1)\} =$$

$$\left( \{500 C_b(o, n)\} + \frac{\Delta t W}{V \rho_f} \left( \{500 C_b(i, n+1)\} + 0.1 \frac{\left( \frac{W_b}{P} \right)}{\left( \frac{P}{5000} \right)} \right) \right) / N$$

$$N = 1 + \frac{\Delta t W}{V \rho_f}$$

Changing to the internal number representation and the unit ppm for boron acid concentration with 2000 ppm equal to the integer 4096 gives:

$$\{2.048 C_b(o, n+1)\} = \{1024 \{2.048 C_b(o, n)\} + \{1024 \frac{\Delta t W}{V \rho_f} \left( \{2.048 C_b(i, n+1)\} + 409.6 \frac{\left( \frac{W_b}{P} \right)}{\left( \frac{P}{5000} \right)} \right)\} \right) / N$$

$$N = 1024 + \{1024 \frac{\Delta t W}{V \rho_f}\}$$

$$\text{with } \{1024 \frac{\Delta t W}{V \rho_f}\} = 69 \frac{\{2048 \left( \frac{W}{5000} \right)\}}{\{200 V\}}$$

for the primary circuit outside the reactor,

$$\text{and } \{1024 \frac{\Delta t W}{V \rho_f}\} = 69 \frac{\{2048 \left( \frac{W_C}{15000} \right)\}}{\{66.67 V\}}$$

for the volumes inside the reactor. The density  $\rho_f$  is taken as the constant value 725 kg/m<sup>3</sup>. The equation can be transformed to

$$\{2.048 C_b(o, n+1)\} = \{2.048 C_b(o, n)\} + \{1024 \frac{\Delta t W}{V \rho_f} \left( \{2.048 C_b(i, n+1)\} - \{2.048 C_b(o, n)\} + 409.6 \frac{\left( \frac{W_b}{P} \right)}{\left( \frac{P}{5000} \right)} \right)\}$$

The last term with  $W_b$  is only present in the boron acid insertion compartment. The previous term

equation is valid for a power station with 3 primary loops with equal coolant flow and with boron acid insertion in all loops. With only one insertion point the constant 409.6 is reduced to 409.6/3, if the maximum insertion rate remains 1 kg/s for that point.

The last equation is the final form for programming.

The calculation routine HYDRA3 contains an array VBO with volume values equal to {200 V} outside the reactor and {66.67 V} inside.

VBO: 235; 235; 1583; 236; 236; 236; 236; 3067; 235; 235; 235; 914; 1045; 1045; 1045; 1045; 914; 246; 246; 235.

The array for the boron acid concentration, CBO, is found in the last file page together with the array CBREST used for accumulated remainder storage. The concentrations are further inserted in the 16 arrays A0-A15 using one compartment over 4 core sections.

The inlet flow of boron acid  $W_b$  goes through AI8. The concentration in the mixing compartment is sent out on MDAC9 with scale factor  $SF C_b = 1/2000$  with ppm as unit.

## 5. THE PRESSURISER MODEL

### Basic data:

Height, inner	11.27 m
Diameter, inner	2.135 m
Volume:	37.8 m <sup>3</sup>
Normal water volume:	22.0 m <sup>3</sup>
Steam-tank surface:	39.0 m <sup>2</sup>
Surge tube:	
Length	13.0 m
Diameter, inner	284.2 mm
Volume	0.825 m <sup>3</sup>

### 5.1. The two-point non-linear model

#### Physical Parameters

$$\rho_{fs} = (-4.79928E-3 \times p - 0.426907) \times p + 775.435$$

$$\rho_{fs} = (5.83223E-3 \times p - 0.684103) \times p + 67.9603$$

$$\frac{d\rho_{fs}}{dp_s} = ((-2.82339E-6 \times p + 1.06286E-3) \times p - 0.135616) \times p + 4.1627$$

$$\frac{d\rho_{gs}}{dp_s} = ((1.94994E-6 \times p - 7.23306E-4) \times p + 9.55994E-2) \times p - 3.63699$$

$$h_{fs} = (2.36941E-6 \times p + 3.34697E-3) \times p + 1.05577$$

$$h_{gs} = (-1.55610E-5 \times p + 1.72963E-3) \times p + 2.705997$$

$$\frac{dh_{fs}}{dp_s} = (2.52025E-7 \times p - 7.1493E-5) \times p + 9.0087E-3$$

$$\frac{dh_{gs}}{dp_s} = ((-3.76728E-9 \times p + 1.42818E-6) \times p - 0.202486E-3) \times p + 8.11117E-3$$

$$\left(\frac{\partial \rho_f}{\partial h}\right)_p = (-1.55056E3 \times h_f + 4.16825E3) \times h_f - 3.20438E3$$

$$\left(\frac{\partial \rho_f}{\partial p}\right)_h = 0.25$$

$$\left(\frac{\partial \rho_g}{\partial h}\right)_p = 0.61E3 \times h_g - 1.74E3$$

$$\left(\frac{\partial \rho_g}{\partial p}\right)_h = -0.7 \times h_g + 2.49$$

$$c_{pg} = 0.010 \text{ MJ/kg}^\circ\text{C} \text{ for steam near saturation}$$

$$\frac{dT_g}{dp_g} = 0.80 \text{ }^\circ\text{C/bar} \text{ for saturated steam}$$

$$C_v = 10 \text{ MJ/}^\circ\text{C} \text{ for the tank wall in constant volume}$$

$$k_{qgv} = 0.2 \text{ MJ/}^\circ\text{C} \text{ for the steam tank wall near saturation}$$

$$h_{fg} = h_{gs} - h_{fs}$$

$$\rho_f = \rho_{fs} + \frac{\partial \rho_f}{\partial h} (h_f - h_{fs})$$

$$\rho_g = \rho_{gs} + \frac{\partial \rho_g}{\partial h} (h_g - h_{gs})$$

The units are:  $\rho$  : kg/m<sup>3</sup>

$h$  : MJ/kg

$p$  : bar

#### Input parameters:

$$h_k = 1.23 \text{ MJ/kg}$$

$$h_i = 1.45 \text{ "}$$

The program is given in appendix H. It is written in the macro language HYBAL for communication with the analog machine and contains 4 FPP-routines and 1 PDP8-code routine.

The PDP8-code routine controls the FPP-routines and takes care of the analog output setting.

FST is a parameter input routine. It may at any time be requested by typing "0" (zero) at the DEC-writer. It must be called once, when the program is started. It is used to define IC values for VF, P, and Q, and further to insert control parameters for Q, WK and WR as used in equations (5.1.8)-(5.1.10).

INPUT is an actuation signal input routine. It follows automatically after FST and may, besides, at any time be called from the DEC-writer by typing "1". It is used to define the input variable  $\Delta W_i$  as either a step- or a ramp-pulse function. DELTA WI = impulse height, DELTA T = impulse width, and STEPSWITCH = 1 gives a step, while STEPSWITCH = 0 gives a ramp-pulse.

FLC is an IC insertion routine; it resets the variables to the values specified in FST and prepares for a transient calculation.

FOP is the main transient calculation routine.

The operation of the program is controlled via the digital inputs DI(0), DI(1) and DI(2). For DI(0) = 1 the program goes to the IC-mode; for DI(0) = 0 and DI(1) = 1 it goes to the operate mode, for which the calculations are synchronized via pulses (100  $\mu$  sec.) on DI(2). As the integration step is 0.1 sec., 10 pulses/sec give real time calculation. A pulse rate of 100 per sec.

may be used to speed up the calculations for slow transients, but 10 pulses/sec. is recommended for short fast transients due to an iterations loop, which is interrupted by the synchronization pulse. 100 pulses/sec. give only time for 2 runs through the loop, resulting in damped oscillations in the time derivative  $\dot{p}$  for step input function.

All output goes through analog channels according to the following list with variables, scale factors, zeropoints and TRAP6 numbers at overflow:

A00: $((p-p_0)/20)$	TRAP6	0
A01: $((V_f-V_{f0})/10)$	"	1
A02: $(W_e/50)$	"	2
A03: $(W_c/50)$	"	3
A04: $(W_k/50)$	"	4
A05: $(W_T/100)$	"	5
A06: $(Q/2)$	"	6
A07: $(\dot{p}/2)$	"	7

The conditions of the water and steam phases are shown by digital outputs. DO(0) = 1 indicates water saturation, and DO(1) = 1 indicates steam saturation.

The program contains the following constants:

$$DT = \Delta t = 0.1$$

$$V = 37.8 \text{ Tank volume}$$

$$HWK = h_k = 1.23$$

$$HWI = h_i = 1.45$$

KRFS: constants for  $\rho_{fs}$

KRGS: " "  $\rho_{gs}$

KRFSP: constants for  $\frac{d\rho_{fs}}{dp}$

KRGSP: " "  $\frac{d\rho_{gs}}{dp}$

KHFS: " "  $h_{fs}$

KHGS: " "  $h_{gs}$

KHFSP: " "  $\frac{dh_{fs}}{dp}$

KHGSP: constants for  $\frac{dh_{gs}}{dp_s}$

KRFH: " "  $\left(\frac{\partial \rho_f}{\partial h}\right)_p$

KRGH: " "  $\left(\frac{\partial \rho_g}{\partial h}\right)_p$

KRGP: " "  $\left(\frac{\partial \rho_g}{\partial p}\right)_h$

RFP =  $\left(\frac{\partial \rho_f}{\partial p}\right)_h$

CPG =  $c_{pg} = 0.01$

DTSP =  $\frac{dT_s}{dp_s} = 0.6$

CV =  $C_v = 10$

KQGV =  $k_{qgv} = 0.2$

SP =  $2048 \times SF_p = 2048/20 = 102.4$

SVF =  $2048 \times SF_v = 2048/10 = 204.8$

SWE =  $2048 \times SF_w = 2048/50 = 40.96$

SWC =  $2048 \times SF_c = 2048/50 = 40.96$

SWK =  $2048 \times SF_k = 2048/25 = 81.92$

SWR =  $2048 \times SF_r = 2048/100 = 20.48$

SQ =  $2048 \times SF_Q = 2048/2 = 1024$

SPP =  $2048 \times SF_p = 2048/2 = 1024$

## 5.2. The simplified pressuriser model

The physical parameters are represented by polynomials of lower degree than used in section 5.1 to save computing time.

$$\rho_{fs} = 602 - 1.82 \times (p-150) = 875 - 1.82 \times p$$

$$\rho_{gs} = 98 + 1.04 \times (p-150) = -58 + 1.04 \times p$$

$$\frac{d\rho_{fs}}{dp_s} = -(1.82 + 0.0092 \times (p-150)) = -(0.44 + 0.0092 \times p)$$

$$\frac{d\rho_{gs}}{dp_s} = 1.04 + 0.0112 \times (p-150) = -0.64 + 0.0112 \times p$$

$$h_{fs} = 1.611 + 0.0040 \times (p-150) = 1.011 + 0.0040 \times p$$

$$h_{gs} = 2.614 - 0.0029 \times (p-150) = 3.049 - 0.0029 \times p$$

$$\frac{dh_{fs}}{dp_s} = 4.0 \text{ E-3}$$

$$\frac{dh_{gs}}{dp_s} = -(2.90 + 0.030 \times (p-150)) \text{ E-3} = (1.6 - 0.030 \times p) \text{ E-3}$$

$$\left(\frac{\partial \rho_f}{\partial h}\right)_p = -(525 + 730 \times (h_f - 1.6)) = 643 - 730 \times h_f$$

$$\left(\frac{d\rho_f}{dp}\right)_h = 0.25$$

$$h_f(W_i) = 1.395 + 0.593 \text{E-2} \times (T-310) = -0.4433 + 0.593 \text{E-2} \times T$$

$$h_f(W_k) = 1.235 + 0.504 \text{E-2} \times (T-280) = -0.1762 + 0.504 \text{E-2} \times T$$

$$T_{sa} = 0.54 \times (p-150) + 324.1 = 261.1 + 0.54 \times p$$

The program is given in appendix A, file PWR2.8B, file pages 2 and 3. File page 2 contains all the numerical data and variables, and file page 3 contains the calculation routine consisting of an IC-routine, PRIC, and an OP-routine, PROP.

The IC values and control parameters are inserted as fixed data. The input variables  $\Delta W_i$ ,  $T_i$  and  $T_k$  are received from the routine FPP2 discussed in section 4.2. The surge flow  $\Delta W_i$  is added to the steady state flow  $W_i(0)$  calculated in the IC routine. For long-term transients a control term,  $\Delta W_i(c)$ , is necessary to keep the water level at a fixed steady state value; it is not included in the present version. The temperatures  $T_i$  and  $T_k$  of the surge flow and the cooling water are used to calculate the corresponding enthalpy values.

The only output value needed by other submodels is the saturation temperature  $T_{ps}$  calculated from the pressure. But other variables are displayed too for operator communication. The output variables with scale factors, zeropoints and overflow numbers are:



AOO :  $((p_p - 150)/20)$  TRAP6 40  
 MDAC10:  $((V_f - 12)/20)$  " 41  
 MDAC11:  $(W_e/50)$  " 42  
 MDAC12:  $(W_c/50)$  " 43  
 MDAC7 :  $((T_{ps} - 300)/100)$  " 44

The iteration mentioned for the more detailed model is not necessary here, as the driving function  $W_i$  has no high frequency components, and the computing time would be unacceptably long too. But there still exists a tendency for oscillations to start, when the water condition shifts between the two states. This is avoided using a digital filter for  $W_e$  with a time lag of 0.2 sec.

The constants in the first file page are:

DT =  $\Delta t = 0.1$

VPR = 37.8 Tank volume

KPP : coefficients for the polynomials:

$$\rho_{fs}, \rho_{gs}, \frac{d\rho_{fs}}{dp_s}, \frac{d\rho_{gs}}{dp_s}, h_{fs}, h_{gs}, \frac{dh_{gs}}{dp_s}, \left(\frac{dp_f}{dh}\right)_p, h_i, h_k$$

$$\text{and } \frac{dT_s}{dp_s}$$

$$\text{HFSP} = \frac{dh_{fs}}{dp_s} = 4.0E-3$$

$$\text{RFP} = \left(\frac{\partial \rho_f}{\partial p}\right)_h = 0.25$$

$$\text{WIKO} = \frac{\Delta t}{\rho_f \times (V_{\text{surge tube}})^{1/3}} = \frac{3 \times 0.1}{725 \times 0.825} = 0.502E-3$$

$$\text{SP} = 2048 \times \text{SF } p_p = 2048/20 = 102.4$$

$$\text{SVF} = 4096 \times \text{SF } V_f = 4096/20 = 204.8$$

$$\text{SWE} = 4096 \times \text{SF } W_e = 4096/50 = 81.92$$

$$\text{SWC} = 4096 \times \text{SF } W_c = 4096/50 = 81.92$$

$$\text{STSA} = 4096 \times \text{SF } T_{ps} = 4096/100 = 40.96$$

NVF = Zerpoint for  $V_f = 12$

VFP = IC value for  $V_f$

P0 = " " " p

Q0 : Control parameters for Q:

IC value = 0.038 MW

Offset = 1 bar

Gain = 0.16 MW/bar

Max.value= 1.3 MW

WKP : Control parameters for  $W_k$ :

IC value: calculated in the PRIC routine

Offset = 1 bar

Gain = 2 kg/s/bar

Max.value= 20 kg/s

WRD : Control parameters for  $W_r$ :

Offset = 10 bar

Max.value= 100 kg/s

## 6. THE STEAM GENERATOR

### Basic data:

$$A_p = 1.035 \text{ m}^2$$

$$A_g = 5.160 \text{ m}^2$$

$$A_r = 4.630 \text{ m}^2$$

$$A_b = 9.770 \text{ m}^2$$

$$A_d = 0.667 \text{ m}^2$$

$$D_{sp} = 0.0197 \text{ m}$$

$$D_{sg} = 0.0436 \text{ m}$$

$$D_{sd} = 0.126 \text{ m}$$

$$\begin{aligned}
 Ar &= 0.00127 \text{ m} \\
 V_p &= 20.9 \text{ m}^3 \\
 V_s &= 52.2 \text{ "} \\
 V_e &= 75.0 \text{ "} \\
 V_r &= 12.6 \text{ "} \\
 V_{bl} &= 18.8 \text{ "} \\
 V_{bh} &= 7.8 \text{ "} \\
 V_d &= 6.94 \text{ "} \\
 V_{pi} &= V_{po} = 4.57 \text{ m}^3 \\
 L_c &= L_d = 10.11 \text{ m} \\
 L_r &= L_b = 2.725 \text{ "} \\
 \Delta x &= \Delta z = 0.5055 \text{ m} \\
 O_p &= 210 \text{ m}^2/\text{m} \\
 O_s &= 237 \text{ "} \\
 O_r &= 223 \text{ "} \\
 \lambda_r &= 0.014 \text{ KW/m}^\circ\text{C} \\
 C_r &= 980 \text{ KJ/m}^\circ\text{C} \\
 S &= 1.5 \\
 At &= 0.05 \text{ s}
 \end{aligned}$$

### 6.1. The detailed one-dimensional model

#### Physical parameters:

$$\begin{aligned}
 T_{sa} &= 137.88 + 5.0121 \times p - 0.79614E-1 \times p^2 + 0.72476E-3 \times p^3 \\
 &\quad - 0.25717E-5 \times p^4 \\
 p_{fs} &= 922.02 + 0.54104 \times T_{sa} - 0.41904E-2 \times T_{sa}^2 \\
 p_{gs} &= -104.953 + 1.53481 \times T_{sa} - 0.768233E-2 \times T_{sa}^2 + 0.141607E-4 \times T_{sa}^3 \\
 \frac{dp_{fs}}{dp_s} &= -33.314 + 0.29584 \times T_{sa} - 0.93865E-3 \times T_{sa}^2 + 0.10129E-5 \times T_{sa}^3 \\
 \frac{dp_{gs}}{dp_s} &= 1.0923 - 0.59817E-2 \times T_{sa} + 0.14787E-4 \times T_{sa}^2
 \end{aligned}$$

$$\begin{aligned}
 h_{fg} &= 1.9912 + 3.2023E-3 \times T_{sa} - 0.17199E-4 \times T_{sa}^2 \\
 \frac{dh_{fs}}{dp_s} &= 0.18065 - 1.7121E-3 \times T_{sa} + 0.56767E-5 \times T_{sa}^2 - 0.64176E-8 \times T_{sa}^3 \\
 \frac{dh_{gs}}{dp_s} &= 0.064714 - 0.63723E-3 \times T_{sa} + 0.20824E-5 \times T_{sa}^2 - 0.23142E-8 \times T_{sa}^3 \\
 c_{pp} &= -0.042044 + 0.20448E-3 \times T_p + 0.77403E-6 \times T_p^2 - 0.28309E-8 \times T_p^3 \\
 &\quad - 0.87750E-11 \times T_p^4 + 0.26327E-13 \times T_p^5 \\
 c_{ps} &= 0.22556E-3 + 0.61417E-4 \times T_{sa} - 0.31531E-6 \times T_{sa}^2 + 0.57419E-9 \times T_{sa}^3 \\
 H_p &= 1.82569 - 0.772876E-2 \times T_p + 0.155828E-4 \times T_p^2 \\
 H_s &= 0.875 + 0.0012 \times (T_{sa} - 250) \\
 \rho_f &= 1740.9 - 9.4540 \times T_p + 0.036496 \times T_p^2 - 0.54202E-4 \times T_p^3
 \end{aligned}$$

The units are  $\text{m}^3$ , kg, bar and MJ except for  $H_p$  and  $H_s$  where KJ is used instead of MJ.

The program, which is written in Fortran IV, is given in Appendix J. It uses 3 device numbers, which must be defined when it is started.

Device no. 7 is the normal output device for the transients. DEC-writer, lineprinter, DEC-tape or disc file may be used.

Device no. 6 is the output device for a new set of IC-values calculated by the program itself. Paper tape, DEC-tape or disc file may be used.

Device no. 5 is the input device for the IC-values needed at start. Paper tape, DEC-tape or disc file may be used.

Device nos. 7 and 5 must always be defined, while a definition for no. 6 is only needed when a new IC-value set is produced. No. 7 is used with option C for a non-file-structured device, such as the DEC-writer, and without option C for a file-structured device. At program start the operator must type some input variables and parameters on request; these are:

WP :  $W_p$ , primary flow

CL :  $C_1$ , steam valve constant

TPI :  $T_{pi}$ , primary inlet temperature

TFI :  $T_{fi}$ , feedwater temperature

NT : Step/ramp indicator. NT = 0 gives a step input; NT = n gives a ramp input of length  $n \cdot \Delta t$ . The input step or ramp may be in any of the 4 variables mentioned above.

M : number of printouts in a transient.

N : number of time intervals  $\Delta t$  between printouts.

It is a good practice to use the same input values as in the IC values for 1 or 2 printouts to check that the IC-conditions are really in a stationary state, and then return to the input section by the following program control facility.

After the last printout, after  $(N \times M \times \Delta t)$  sec. problem time, the program asks for a continuation input switch:

1. Stop the program.
2. Start with new input variables.
3. Continue the transient calculation with new values of M and N.
4. Write a new set of IC values on the output file specified by the start.
5. Type a profile table on device no. 7.

An example of the output is given in appendix J. It is shown how the program is started and the different control switches are used. The profile printout contain 8 columns with a line for each core section, so 2 columns are used for  $T_p$ ,  $T_{r1}$  and  $T_{r2}$ . The extra lines for  $T_s$  and  $T_p$  give the inlet temperatures and the temperature in the primary inlet and outlet chamber.

The calculation time is about 15 sec. for 1 sec. problem time.

The program contains a head with DATA specifications of main parameters. These are:

AS =  $A_s$     AP =  $A_p$     AR =  $A_r$     AF =  $A_b$     AD =  $A_d$   
 LC =  $L_c$     LR =  $L_r$     LF =  $L_b$     DZ =  $\Delta z$   
 OS =  $O_s$     OP =  $O_p$     OR =  $O_r$   
 $\sqrt{R} = V_r$     VE =  $V_e$     VFL =  $V_{b1}$     VFH =  $V_{bh}$   
 VDO =  $V_d$     VPI =  $V_{pi} = V_{po}$   
 DEP =  $D_{ep}$     DES =  $D_{es}$     DED =  $D_{ed}$     DR =  $\Delta r$   
 GH =  $g \cdot \Delta x$     CRH =  $C_r/2$     LAR =  $\lambda_r$     CPR =  $c_{pm}/c_{ps}$   
 S = S    DT =  $\Delta t$

## 6.2. The simplified steam generator model

The basic data are the same as for the detailed model, but several physical data are used as constant values. The simplifications and consequences are most conveniently discussed for each equation separately, as the same parameter may have quite different influence in two equations. All the equations are given with numerical values, those containing only basic data without comments.

Eq. (6.2.1a):  $\rho_f = 725 \text{ kg/m}^3$ . Variations only have influence on a time lag, while variations in  $c_{pp}$  have a strong influence on the heat delivery to the secondary side. Therefore a temperature dependent representation of  $c_{pp}$  is important:

$$c_{pp} = 0.026285 - 0.16617E-3 \times T_p + 0.32291E-6 \times T_p^2$$

$$\Delta T_{po} = 0.660E-4 \times \left( \frac{Q_p}{c_{pp}} - W_p \Delta T_{po} \right). \quad (6.2.1a)$$

$$T_{po} = T_{p1,n} - \Delta T_{po}. \quad (6.2.1)$$

Eq. (6.2.1b) and (6.2.1c) are included in the calculations of the primary loop temperature as described in section 4.2.

Eq. (6.2.2):  $a_p = 0.41$

$$T_p = 0.41 T_{p1} + 0.59 T_{po}. \quad (6.2.2)$$

$$T_{r1} = 0.1009 (Q_p - Q_r). \quad (6.2.3)$$

$$T_{r2} = 0.1009 (Q_r - Q_s). \quad (6.2.4)$$

Eq. (6.2.5): The heat transfer parameter  $H_p$  is equal to 0.92  $\pm$  0.03 in the temperature range  $300 \pm 20^\circ \text{C}$  so it is used with the constant value 0.92

$$Q_p = 0.1917 W_p^{0.8} (T_p - T_{r1}). \quad (6.2.5)$$

$$Q_r = 49.71 (T_{r1} - T_{r2}) \quad (6.2.6)$$

Eq. (6.2.7): The term  $\exp(p/43.4)$  will vary in the range 0.1 to 1.0 but as the temperature difference  $(T_{r2} - T_{ss})^2$  is very small it is small due to the quadratic term, it is an overestimate to set  $(p/43.4)$  equal to 4.6. The error in  $T_{po}$  will be about 1.5

for the greatest pressure deviation, which is regarded as insignificant compared to the variation in saturation temperature over the range 260 - 290 °C.

$$Q_s = 42.53(T_{r2} - T_{ss})^2. \quad (6.2.7)$$

Eq. (6.2.8):  $c_{ps} = 0.0052 \text{ MJ/kg}^\circ\text{C}$  with an error less than 10%. The influence on  $Q_k$  will be much smaller as the second term is only about 10% of  $Q_s$ .

$$Q_k = Q_s - 0.0052 W_s(T_{ss} - T_d) \quad (6.2.8)$$

Eqs. (6.2.9): The equation has 3 parameters dependent on temperature and load, as the total coefficient to  $\dot{p}$  is regarded as one parameter.  $\rho_{gs}$  varies in the range 25 - 40 kg/m<sup>3</sup>, but is used as a constant equal to 33 kg/m<sup>3</sup>, because it only has influence on the time constant for  $V_g$ , which anyway is small compared with the dominating time constant for the total system.  $h_{fg}$  as coefficient for  $Q_k$  is rather important, as it determines the steady-state value of the steam production when  $Q_k$  is given; so a second degree polynomial is used:

$$h_{fg} = 1.9912 + 0.32023E-2 \times T_{ss} - 0.17199E-6 \times T_{ss}^2$$

The coefficient D for  $\dot{p}$ :

$$D = \frac{1}{h_{fg}} \left( V_g (\rho_{gs} \frac{dh_{fg}}{dp_s} + h_{fg} \frac{d\rho_{gs}}{dp_s}) + V_f \rho_{fs} \frac{dh_{fg}}{dp_s} - V_s \right)$$

has been calculated for several steady-state load levels using results obtained by the detailed program. The coefficient is included in table C.2 in appendix C. It appears to be fairly constant in the load range 25 - 115% of full load. For a transient state it may run outside the range 90 - 108 kg/bar shown in the table, but it is still used as a constant equal to 98 based on the same argumentation as used above for  $\rho_{gs}$ .

$$\dot{V}_g = 0.3 \left( \frac{Q_k}{h_{fg}} - 98 \dot{p}_s - W_g \right) \quad (6.2.9)$$

or normalized with respect to  $V_g$ :

$$\frac{\dot{V}_g}{V_g} = \dot{U} = 0.580E-3 \frac{Q_k}{h_{fg}} - 0.0570 \dot{p}_s - 0.58E-3 W_g. \quad (6.2.9)$$

Eq. (6.2.10): The coefficient  $(\rho_{fs} - \rho_{gs})$  varies in the range 690 - 760 kg/m<sup>3</sup>, so a constant value equal to 725 kg/m<sup>3</sup> is used. The coefficient E:

$$E = V_g \frac{d\rho_{gs}}{dp_s} + V_f \frac{d\rho_{fs}}{dp_s}$$

is shown in the table C.2. The working range appears to be -(40 - 70) kg/bar. Even the variation is quite large, the same argumentation as used above for  $\rho_{gs}$  justifies the selection of a constant value of 52 kg/bar.

$$W_f = W_s - W_g + 725 \dot{V}_g + 52 \dot{p}_s \quad (6.2.10)$$

or normalized with respect to  $V_g$ :

$$W_f = W_s - W_g + 37800 \dot{U} + 52 \dot{p}_s. \quad (6.2.10)$$

Eq. (6.2.11):  $\rho_{gs}/\rho_{fs}$  is important for the determination of the void fraction  $\alpha$ , so a second-degree polynomial is used.

$$10 \frac{\rho_{gs}}{\rho_{fs}} = 0.14201E-2 + 0.51861E-2 \times p_s + 0.26371E-4 \times p_s^2.$$

The slip ratio S is used as a constant 1.5, as for the detailed model.

$$W_g = 1.5 W_f \frac{\alpha}{1-\alpha} \frac{\rho_{gs}}{\rho_{fs}}. \quad (6.2.11)$$

Eq. (6.2.12): The function  $F_g(V_g)$  is shown in the table C.2 and plotted in Ref. 1, fig. 12. A straight line gives a reasonable representation of the calculated values.

$$\alpha = (2.33 - 1.7 \frac{V_g}{V_s}) \frac{V_g}{V_s}. \quad (6.2.12)$$

Eqs. (6.2.13) - 6.2.16): The steam transit time varies between 0.5 and 1.5 sec. according to the table C.2. However, as a rule

appears as a dynamic correction term for  $p$  and  $W_b$ , a constant value of 1.0 sec. will be used. From the table the working range for C1 is found to be 27 - 30 kg/bar, which justifies the selection of a constant value of 28 kg/bar. The denominator in eq. (6.2.15) is given as C2 in the table C.2. It varies in the range 73 - 78 kg/bar, so a constant value equal to 75 is reasonable. Finally,  $\rho_{fs}$  and  $\rho_{gs}$ , in connection with  $V_r$  in eqs. (6.2.15) and (6.2.16), are taken as constants:  $\rho_{fs} = 750$  and  $\rho_{gs} = 33$  kg/s.

$$\dot{\alpha}_r = \alpha - \alpha_r \quad (6.2.14)$$

$$\dot{p}_s = (W_g - W_l - 416\dot{\alpha}_r)/75 \quad (6.2.15)$$

$$W_b = W_f + 28\dot{p}_s + 9450\dot{\alpha}_r \quad (6.2.16)$$

Eqs. (6.2.17) and (6.2.18):  $\rho_{fs} = 750$  kg/s and  $c_{pm}/c_{ps} = 0.94$ .

$$\dot{T}_b = 0.709E-4 \times (W_b(T_{ss} + T_b) - 0.94 W_i(T_b - T_i)) \quad (6.2.17)$$

$$\dot{T}_d = 1.921E-4 \times W_s(T_b - T_d) \quad (6.2.18)$$

Eqs. (6.2.19) - (6.2.21):  $F_f = 0.0425$ . The function  $F_R(V_g)$  is tabulated in table C.2 and plotted in Ref. 1, fig. 12. In the working range the straight line  $F_R = 77 V_g/V_s$  is a usable approximation even though the curve must end in  $ER\Delta x = L_c = 10.11$  for  $V_g = 0$ .  $EL_{xc}/A_x = 12.1$  and  $V_{fi} = V_{dA_d}/A_s$

$$\frac{\Delta p_1}{\rho_{fs}} = 0.341 \frac{V_g}{V_s} v_d^{1.8} \quad (6.2.19)$$

$$\frac{\Delta p_2}{\rho_{fs}} = 0.866 v_d^{1.8} \quad (6.2.20)$$

$$\dot{v}_d = 0.0826(99.34 \frac{V_g}{V_s} - (\frac{\Delta p_1}{\rho_{fs}} + \frac{\Delta p_2}{\rho_{fs}})) \quad (6.2.21)$$

Eqs. (6.2.22) and (6.2.23):  $\rho_{fs} = 750$  kg/s and the coefficient for  $p$  is taken as -75 kg/bar, as the variation of  $\pm 10\%$  in the working range is without any influence on the other equations.

$$W_s = 515 V_d \quad (6.2.22)$$

$$\dot{L}_b = 0.136E-3 \times (W_b + W_i - W_s - 75\dot{p}_s) \quad (6.2.23)$$

The model is implemented as an analog model with the 3 coefficients  $c_{pp}$ ,  $h_{fg}$  and  $(10 \rho_{gs}/\rho_{fs})$  calculated in a digital routine and inserted via MDACs. The analog diagram is given in appendix C together with the scaled equations, potentiometer listing and DFG tables. Included are also 2 tables which have been used for evaluation of the coefficients. Table C.1 gives some physical parameters in the actual temperature range, and table C.2 gives a set of variables calculated by the detailed model together with some main parameters.

The digital routine for parameter calculation is found in FPP2 together with the primary temperature calculation. The input variables are inserted in the PDP8 routine HYDRA2. These are:

$$AI12: [(p_s - 60)/25]$$

$$AI13: [(T_{ss} - 250)/50].$$

The analog model receives 2 temperatures from the primary temperature routine:  $T_{p1}$ , the temperature in the inlet chamber, and  $T_{p1,2}$ , the temperature in the second of the U-tube compartments. These temperatures are set on analog outputs in the PDP8 routine HYDRA5 together with the adjustment of the MDACs. The output variables with TRAP6 numbers at overflow are:

$$AO6 : [(T_{p1} - 300)/50] \quad \text{TRAP6} \quad 21$$

$$AO7 : [(T_{p1,2} - 300)/50] \quad \text{TRAP6} \quad 22$$

$$MDAC2: [0.5759/250 c_{pp}] \quad " \quad 24$$

$$MDAC3: [0.580/h_{fg}] \quad " \quad 25$$

$$MDAC4: [10 \rho_{gs}/\rho_{fs}] \quad " \quad 26$$

$$MDAC13: [(T_{p2} - 250)/100]$$

The first file page of PWR2.6B contains some constants belonging to the parameter calculation. These are:

CFFK: coefficients for  $c_{pp}$

HFGK: " "  $h_{fg}$

RGFK: " "  $10 \rho_{gs}/\rho_{fs}$

$$SFFK: 1/(2048 \times 37 p_s) = 25/2048 \times 0.012287$$

$$SFTIN: 1/(2048 \times 37 T) = 50/2048 \times 0.012287$$

$$\begin{aligned} \text{SFDP4: } 4096 \times \text{SF } (1/c_{pp}) &= 4096 \times 0.5759/250 = 9.4355 \\ \text{SFDP5: } 4096 \times \text{SF } (1/h_{fg}) &= 4096 \times 0.580 = 2375.68 \\ \text{SFDP6: } 4096 \times \text{SF } (10 \rho_{gs}/\rho_{fs}) &= 4096 \\ \text{SFTUD: } 2048 \times \text{SF } T &= 2048/50 = 40.96 \end{aligned}$$

## 7. THE TURBINE-REHEATER MODEL

### Basic data:

#### Turbine:

$$\begin{aligned} V_h &= 10 \text{ m}^3 \\ V_l &= 50 \text{ m}^3 \\ k_v &= 51.30 \text{ kg/s bar} \\ k_h &= 25.95 \text{ kg/s bar} \\ k_l &= 73.50 \text{ kg/s bar} \\ a_h &= 0.138 \\ \beta_h &= 0.935 \\ \beta_l &= 0.948 \\ \gamma_h &= 0.8 \\ \gamma_l &= 0.8 \\ \gamma_g &= 0.95 \\ \frac{dp_g}{dp} &= 0.5 \text{ kg/m}^3 \text{ bar} \end{aligned}$$

#### Reheater:

$$\begin{aligned} \text{Tube dimensions: } 22/18 \text{ mm} \\ \text{Heating surface} &= 6000 \text{ m}^2 \\ \text{Tube weight} &= 80 \text{ t} \\ \text{Tube heat capacity } C_t &= 33 \text{ MJ/}^\circ\text{C} \\ \text{Volume outside tube } V_r &= 50 \text{ m}^3 \\ \text{Tube heat transfer constant: } 45 \text{ MW/}^\circ\text{C} \end{aligned}$$

$$\begin{aligned} \text{Heat transfer constant hot side: } 45 \text{ MW/}^\circ\text{C} \\ \text{Heat transfer constant cold side: } 11.4 \text{ MW/}^\circ\text{C} \\ k_t &= 22.5 \text{ MW/}^\circ\text{C} \\ k_r &= 11.4 \text{ MW/}^\circ\text{C} \\ h_{fg} &= 1.57 \text{ MJ/kg} \\ c_p \text{ for superheated steam} &= 0.0025 \text{ MJ/kg}^\circ\text{C} \\ \rho_g &= 5 \text{ kg/m}^3 \end{aligned}$$

The pressure dynamics and the reheater equations are implemented as an analog model, while the turbine power calculation is made in a digital routine. The equations for the analog part with numerical values are:

$$\dot{p}_h = 0.20(G_v - G_h) \quad (7.1)$$

$$\dot{p}_l = 0.04(0.862(1 - a_t)G_h - G_l) \quad (7.2)$$

$$G_v = 51.3 A_v p_v Y(p_h/p_v) \quad (7.3)$$

$$G_h = 25.95 p_h \quad (7.4)$$

$$G_l = 73.50 p_l \quad (7.5)$$

$$T_{t1} = T_{ps} - 2 \quad (7.21)$$

$$Q_t = 22.5(T_{t1} - T_{t2}) \quad (7.22)$$

$$Q_r = 11.4(T_{t2} - T_{ro}) \quad (7.23)$$

$$T_{t2} = 0.0303(Q_t - Q_r) \quad (7.24)$$

$$T_{ro} = 1.6(Q_r - 0.0025G_r(T_{ro} - T_{r1})) \quad (7.25)$$

$$G_l = G_v + 0.637 Q_r \quad (7.26)$$

The analog diagram, scaled equation, potentiometer list and DFG table are given in Appendix D. The communication with the digital routine for power calculation is described below.

### Turbine power calculations:

The calculations are carried out strictly according to the formulae (7.6) - (7.20) in a digital routine TURB following entry in file PWR.88. The physical parameters are calculated as nominals as follows:

$$T_s = 87.4263 + 19.8697 \times p_s - 1.8237 \times p_s^2 + 0.955588E-1 \times p_s^3 \\ - 0.195821E-2 \times p_s^4 \quad \text{for } 2 < p_s < 17 \text{ bar}$$

$$T_s = 123.752 + 7.14733 \times p_s - 0.182786 \times p_s^2 + 0.270145E-2 \times p_s^3 \\ - 0.156422E-4 \times p_s^4 \quad \text{for } 7.5 < p_s < 60 \text{ bar}$$

$$h_{fs} = -83.7618 + 5.55901 \times T_s - 0.785461E-2 \times T_s^2 + 0.173185E-4 \times T_s^3$$

$$h_{gs} = 2672.52 - 0.841164 \times T_s + 0.141137E-1 \times T_s^2 - 0.347827E-4 \times T_s^3$$

$$s_{fs} = -0.236725E-1 + 0.153926E-1 \times T_s - 0.245531E-4 \times T_s^2 \\ + 0.322284E-7 \times T_s^3$$

$$s_{gs} = 8.77514 - 0.185358E-1 \times T_s + 0.460689E-4 \times T_s^2 - 0.614785E-7 \times T_s^3$$

The energy unit is here kJ; all the constants and the internal calculations in TURB are in kJ, but the input-output variables are in MW.

The FPP routine TURB receives 3 variables from the analog turbine model via the PDP8 routine HYDRA3. These are:

$$AI16: \{P_h/100\}$$

$$AI17: \{P_1/20\}$$

$$AI18: \{Q_r/250\}$$

The output variables with overflow TRAP6 numbers are:

$$AO4: \{(T_{ri} - 175)/50\} \quad \text{TRAP6 } 32$$

$$MDAC6: \{E_g/1000\} \quad \text{" } 31$$

$$MDAC5: \{(1-a_h)(1-a_t)k_h/v_1 \frac{dp_g}{dp_h}\} \\ = \{0.8948 (1-a_t)\} \quad \text{TRAP6 } 33$$

$T_{ri}$  and MDAC5 are used in the turbine analog model, while  $E_g$  on MDAC6 is used in the power grid analog model.

The TURB routine has a head with the following constants:

$$GMH: \gamma_h = 0.8$$

$$GML: \gamma_l = 0.8$$

$$GMG: \gamma_g = 0.95$$

$$KHx: k_h(1-a_h) = 22.369$$

$$SFSC: s_{fs} \text{ for condenser} = 0.4763$$

$$SFGSC: (s_{gs} - s_{fs}) \text{ for condenser} = 7.9197$$

$$HFSC: h_{fs} \text{ for condenser} = 137.77$$

$$HFGSC: (h_{gs} - h_{fs}) \text{ for condenser} = 2423.8$$

$$KHBH: k_h \beta_h = 24.263$$

$$KLBL: k_l \beta_l = 69.678$$

$$SPH: 1/(2048 \times SF p_h) = 100/2048 = 0.048828$$

$$SPL: 1/(2048 \times SF p_l) = 20/2048 = 0.0097656$$

$$SQR: 1000/(2048 \times SF Q_r) = 1000 \times 250/2048 = 122.07$$

$$SKV: 4096 \times SF (1-a_g) = 4096 \times 0.8948 = 3664.92$$

$$SEG: 4096 \times SF E_g/1000 = 4096/(1000 \times 1000) = 0.004096$$

$$STRI: 2048 \times SF T_{ri} = 2048/50 = 40.96$$

$$NTRI: \text{zeropoint for } T_{ri} = 175$$

$$KHFS: \text{coefficients for } h_{fs}$$

$$KHGS: \text{coefficients for } h_{gs}$$

$$KSFS: \text{coefficients for } s_{fs}$$

$$KSGS: \text{coefficients for } s_{gs}$$

$$KTH: \text{coefficients for } T_s \text{ high pressure}$$

$$KTL: \text{coefficients for } T_s \text{ low pressure}$$

### C. THE ELECTRICAL POWER GRID

#### Basic data:

$$S_r = 2$$

$$t = 7.5 \text{ s}$$

$$\tau_{2v} = 0.25 \text{ s}$$

$$\begin{aligned} \tau_{2t} &= 0.5 \text{ s} \\ E_n &= 5000 \text{ MW} \\ E_1 \text{ full load} &= 870 \\ E_2 \text{ normal} &= 4130 \text{ MW} \\ \delta_2 &= 0.1 \\ k_{e2} &= 1 \text{ s}^{-1} \\ k_{e1} &= 0.004 \text{ MW}^{-1} \end{aligned}$$

Max. valve speeds:

PWR plant turbine: Full stroke in 2.5 s  
Base plant turbine: Full stroke in 10 s.

The equations with numerical values are:

$$\frac{\Delta f}{f_n} = \frac{0.5}{1 + 7.5 \text{ s}} \frac{\Delta E}{E_n} \quad (8.5)$$

$$\frac{\Delta E_2}{E_2} = \frac{\Delta f (10 \text{ s} + \frac{1}{s})}{(1 + 0.25 \text{ s}) (1 + 0.5 \text{ s})} \quad (8.6)$$

$$\frac{\Delta E}{E_n} = 0.85 \frac{\Delta E_2}{E_2} + \frac{\Delta E_1}{5000} + \frac{\Delta E_1}{5000} \quad (8.7)$$

$$A_v = 0.004(E_1 - E_{1r}) \quad (8.8)$$

The analog diagram and potentiometer list are given in appendix E.

### 9. FILE INPUT-OUTPUT ROUTINES

The routines that perform the input-output functions mentioned in chapter 1 are described here in some detail.

The test routine that is initiated by typing "0" on the DEC-writer is a standard routine from the HYBAL subroutine library SLIP, so it is not contained in the program listing. It may be used to type and change any floating point number addressed by its octal address. It is not discussed here, as it belongs to the HYBAL library system.

The IC-data output and input routines are built up around the same skeleton. There are two data lists, one for floating point data, ICLIF, and one for 12-bit integers, ICLIH. Both routines have a PDP8-code and a FPP-code section, which transfer data between the core resident program and the disc file PWR.IC according to the two lists. Each list contains a set of specifications consisting of a number followed by an address. The number gives the number of successive data to transfer with the following address as the address of the first data.

The IC output routine has a PDP8-section, ICUD, in file PWR.8B and a FPP-section, ICOUT, in file PWR3.8B. The ICUD routine reads the regulating rod position via AI7, so the reference voltage on the analog machine must be on, when the IC output routine is requested. When finished, the routine gives a message: IC DATA TIL FILE PWR.IC on the DEC-writer.

The IC input routine, which is initiated when DI(11) is set, has a PDP8-section, ICIND, in file PWR.8B and a FPP-section, ICIN, in file PWR3.8B. The routine informs the operator of the regulating rod position and the power reference value, as stored in the IC-data. The ICIND routine adjusts some analog outputs and MDACs according to the IC-data just inserted, and ends with the message: IC DATA IND FRA FILE: PWR.IC.

Reactor static data for new working conditions are inserted from a disc file PWR.ST by the PDP8-routine STAT and the FPP-routine STATF in files PWR.8B and PWR3.8B respectively. File PWR.ST is generated by a Fortran IV program and contains 14 records, the first 13 records with one array each, the last one with 3 numbers. The arrays are:  $\beta$ ,  $N$ ,  $T_u$ ,  $T_{ca}$ ,  $T_c$ ,  $\alpha$ ,  $\rho_m$ ,  $C_1$ ,  $C_2$ ,  $C_3$ ,  $\lambda_n C_n$ , CCR (coarse control rod densities) and  $I_a$ -xenon. The numbers in the last record are regulating rod position and weighting factor, and boron acid concentration. The data is stored in internal code in PWR.ST. The distribution within the core resident program PWR.SV is mainly carried out in the STATF routine, but the final positioning of the regulating rod densities and the boron acid concentration is done in the STAT routine, which also adjusts some analog outputs and MDACs to standard values in order to obtain reasonable start conditions. Further the relative power level is calculated and typed out on the DEC writer together with the regulating rod position. (The full power level is set point at 2600 MW). The routine ends with the message: STATF END PWR.



FILE PWR.ST.

The logging of variables initiated by typing "3" on the DEC-writer is accomplished by the FPP-routine FLOG in file PWR3.8B. The programming is a straight-forward process, as the data must be handled individually. An output example is given in Appendix L.

The input-output routines contains only few constants that may be changed:

FULL in STAFF: Full reactor power/100

NUF in FLOG:  $V_f A/v = 2.18E-11$  for conversion of fission rate to thermal power

KH in FLOG:  $k_h$  for the turbine

HFOQR in FLOG:  $h_{fs}$  for the turbine reheater

REFERENCES

1. P. la Cour Christensen: Description of the Real Time Power Plant Model PWR-PLASIM, Risø Report No. 318 (1975).
2. DOCKET 50-280, SURRY-1, Final Safety Report.
3. DOCKET RESARA, Vol. 3 & 4.
4. P. Skjerk Christensen: A Static One Dimensional Reactor Model, Risø-M-1774.

APPENDIX A

Digital program listing for the power station model.



[illegible]

FORHOLD HAIS RESISTION DIVISION 2  
C BOB NEG

KONCENTRATION I SEKTIONENE  
MC LOWEY PL 600087 OFFER PL  
CONCENTRAREN SEKT I FORDS ANSTALT  
NÆST ARBEJDE FOR BOK KONCENTRATION  
I PATRIAL CONCENTR NED CBO  
MEMBER=200 I SEKTIONER FOR CBO  
1965-1965, 914, 246, 246, 215  
12, 1503, 216, 216, 216, 1967, 215, 215, 215

/KONCENTRATION I 1 MF SECTION  
/KONCENTRATION I 8 MC SEKTIONER  
/KONCENTRATION I 32 MF SEKTIONER  
/INDSÆT BOR KONCENTRATION I NO-MI

[illegible]

EFFICIENT

SUBROUTINE  
HIC. 0  
BANOUT 5.40+2  
CLA  
DCC  
IC SIGNAL  
000 5000  
JMS TRVENT  
15 FIRST 1 STORE IC SLUT  
000 2000  
INDLRES P0 INDL08  
BANIN 5  
CIA  
DCA AB+4  
BANOUT 5.40  
JMP I HIC

OPDA. 0  
CLA  
TAD 11  
TAD 14  
DCA 11  
TAD SEKTA  
TAD ST  
SHA CLA  
JMP I OPDA  
TAD HJ0+1  
JMS DIV1.24  
TAD I 20  
ISZ 20  
TAD HJ0+2  
JMS DIV1.4  
TAD I 20  
DCA I 20  
ISZ 20  
TAD HJ0+3  
JMS DIV1.5  
DCA OPDA1  
TAD OPDA1  
TAD HIC  
DCA HIC  
TAD OPDA1  
TAD I 20  
DCA I 20  
ISZ 20  
TAD HJ0+4  
JMS DIV1.5  
TAD I 20  
DCA I 20  
ISZ 20  
TAD HJ0+5  
CIA  
DCA I 20  
TAD 20  
TAD 14  
DCA 20  
TAD HJ0  
JMS DIV1.12  
TAD 0K  
DCA 0K  
JMP I OPDA  
OPDA. 0

TRVENT. 0  
DIC  
CLA CLL  
DIRC  
AND (2008  
52H CLA  
JMP -3  
JMP I TRVENT  
FEJL0 0TYPEC (NEG WC)  
FEJL1 0TYPEC (NEG WP)  
FEJL4 0TYPEC (STAMPPOS NEG.)  
FEJL5 0TYPEC (DIV OVERFL BOK)  
FEJL6 0TYPEC (C-BOK NEG.)  
FEJL7 0TYPEC (CFOR LANG REGNETID)

PAGE

ICDATA UOLRESNING PRA FILE PNR. IC  
ICUD. FPPST  
RAR  
SZL CLA  
JMP -3  
DCA FPPSI  
FPICL  
BANIN 7. INDEKS  
TAD (FPPD)  
JMS ENTER  
START UPKAPNING AF FPP-TAL  
00PPST: ICOUT.200  
00PPH  
TAD (BUFFER  
JMS WRITE  
CLA  
TAD (ICLIN-1  
DCA 10  
TAD (BUFFER-1  
DCA 11  
TAD (-401  
DCA 20  
TAD I 20  
ISZ 20  
TAD (ICLIN-1  
DCA 10  
TAD (BUFFER-1  
DCA 11  
TAD (-401  
DCA 20  
TAD I 10  
ISZ 20  
TAD (BUFFER  
JMS READ  
CLA  
TAD (ICLIN-1  
DCA 10  
TAD (BUFFER-1  
DCA 11  
TAD (-401  
DCA 20  
TAD I 10  
ISZ 20  
TAD (BUFFER  
JMS READ  
CLA  
TAD (BUFFER-1  
DCA 11  
TAD (-401  
DCA 20  
DCA 10  
TAD I 11  
DCA 0  
DCA I 12  
ISZ 21  
JMP ICIND2  
TAD FILE PNR. IC  
TAD TIL UOLRESNING PRA DISK

LISTE NED ICDATA OG INPUT DATA PRA 12 BIT FORM  
ICLIN. 1. SUMN  
20. N  
26. CBO  
26. CBREST  
10. APD  
10. TAD  
10. INK  
200. AB  
0  
PAGE  
ICINDLRESNING PRA FILE PNR. IC  
ICIND. CLA  
TAD ICIND1  
SHA CLA  
JMP H1  
FPPST  
RAR  
SZL CLA  
JMP -3  
DCA FPPSI  
FPICL  
TAD (FPPD  
JMS LOOKUP  
CLA  
TAD (BUFFER  
JMS READ  
START UPKAPNING AF FPP-TAL  
00PPST: ICIN.200  
00PPH  
TAD (BUFFER  
JMS READ  
CLA  
TAD (ICLIN-1  
DCA 10  
TAD (BUFFER-1  
DCA 11  
TAD (-401  
DCA 20  
ICIND1. TAD I 10  
SHA  
JMP ICIND2  
CIA  
DCA 21  
TAD I 10  
TAD (-1  
DCA 12  
ICIND2. ISZ 20  
JMP -10  
TAD (BUFFER  
JMS READ  
CLA  
TAD (BUFFER-1  
DCA 11  
TAD (-401  
DCA 20  
DCA 10  
TAD I 11  
DCA 0  
DCA I 12  
ISZ 21  
JMP ICIND2



SFU. F - 24414 / -500/2040 SKALAFAKTOR TU IND  
 SFTC. F 024414 / 50/2040 DO TC  
 SFRO. F 24414E-3 / 5/2040 DO RO  
 SFRO. F 40829 / 2000/4086 DO BOR  
 SFCH. F 0.2087E-3 / - 25/2045 DO REG STANG  
 PHIRIN. F 1 E10  
 XX1. F 0  
 XX2. F 0  
 /  
 CCR. F 0  
 REPEAT 17  
 F 375  
 CJI. F 0  
 REPEAT 17  
 F 0  
 CJJ. F 0  
 REPEAT 17  
 F 0  
 CJK. F 0  
 REPEAT 17  
 F 0  
 PHI. F 0  
 REPEAT 17  
 F 0  
 FNP. F 0  
 REPEAT 17  
 F 0  
 NVSF. F 0  
 REPEAT 17  
 F 0  
 SAZE. F 0  
 REPEAT 17  
 F 0  
 SLCH. F 0  
 REPEAT 17  
 F 0  
 CN1. F 0  
 REPEAT 17  
 F 0  
 CN2. F 0  
 REPEAT 17  
 F 0  
 CN3. F 0  
 REPEAT 17  
 F 0  
 /  
 SFN. F 1.7033E-10 / 2.10E-11+4086/500 SKALAFAKTOR N UD  
 F2040. F 2040  
 F4086. F 4086  
 /  
 KONSTANTER FOR FORSINKEDE NEUTRONER  
 LR1. F 1.82 /LAMBDA1  
 LR2. F 2.09  
 LR3. F 0.2000  
 CMH2. F 0.33101 /((2-LR1+DT))/((2-LR1+DT))  
 CMH3. F 1.023399E-4 /((2-BETAL+DT))/((2-LR1+DT))  
 CMH2. F 0.72006  
 CMH3. F 3.406451E-4  
 CMH2. F 3.997124  
 CMH3. F 1.616339E-4  
 CMH1. F 0

# BEREGN KOEFFICIENTER TIL DIFFUSIONSLIGNING

FPP1. STARTF  
 INDEX 0  
 SETB KD /SEKTION 1--14  
 SETX R0+10.JSA KOEF  
 SETX R0+20.JSA KOEF  
 SETX R0+30.JSA KOEF  
 SETX R0+40.JSA KOEF  
 SETX R0+50.JSA KOEF  
 SETX R0+60.JSA KOEF  
 SETX R0+70.JSA KOEF  
 SETX R0+80.JSA KOEF  
 SETX R0+90.JSA KOEF  
 SETX R0+100.JSA KOEF  
 SETX R0+110.JSA KOEF  
 SETX R0+120.JSA KOEF  
 SETX R0+130.JSA KOEF  
 SETX R0+140.JSA KOEF  
 SETX R0+150.JSA KOEF  
 SETX R0+160.JSA KOEF

BASE KD0  
 SETB KD0  
 SETX R0 /SEKTION 0  
 JSA KOEF0  
 FLDR XX1  
 FSTA CJK  
 SETX R15 /SEKTION 15  
 JSA KOEF0  
 FLDR XXI  
 FSTA CJI+55  
 JA LOES

//  
 DEFINITION AF MAKRO TIL POLYNOMBEREGNING  
 ODEF OPRAN:K,KX,N  
 OSET QA=N  
 FLDR KX  
 FFUL FTC  
 FADD KX+3  
 FFUL FTC  
 FSTA K  
 FLDR KX+6  
 FFUL FRO  
 FADD KX+11  
 FFUL FRO  
 FADDN K  
 FLDR KX+14  
 FFUL FRO  
 FADD KX+17  
 FFUL FRO  
 FADDN K  
 FLDR KX+22  
 FFUL FCR  
 @TNE @A.1  
 FADD KX+25  
 FADDN K  
 @TNE @A.6  
 FLDR KX+25  
 FFUL FTU  
 FADD KX+30  
 FFUL FTU  
 FADD KX+33  
 FADDN K

PARAM0  
 //  
 SUBROUTINE TIL KOEFFICIENT BEREGNING  
 BASE KD

KOEF. JA 0  
 ONSNET TU.TC.RD.BOR.CRPOS.TIL FLORING FORM  
 /  
 OPLANT:0.SFTC.HPTC.FTC  
 OPLANT:2.SFTC.HPTC.FTC  
 OPLANT:4.SFRD.HPRO.FRO  
 OPLANT:3.SFRD  
 JOE +3.FPRO F2000  
 FPRO HPRO.FSTA FRO  
 OPLANT:6.SFRCCCR.7.FCR  
 /  
 UDREGN 0  
 OPRAN:0.KD.1  
 UDREGN HV+SIGNAF-SIGNNA  
 OPRAN:0A.KSFA.1  
 UDREGN HV+SIGNAF  
 OCL:KSF+70+(KSF+3)+FROINSF  
 OCL:CCSF+6)+FROINSF:(KSF+11)+FCR+(KSF+14)+NSF:NVSF.7)  
 OCL:COBETW+SAZE.7-05A0  
 UDREGN C(J.3-1).C(J.3).C(J.3+1)  
 OCL:C(402+C(J.7)C(J.7)+5-SR(CJJ.7)  
 JA CCF7  
 /  
 SUBROUTINE TIL KOEF.BEREGNING I SEKTION 0 OG 15  
 BASE L00  
 UDREGN. JA 0 /ONSNET FRA HELLTA  
 OPLANT:0.SFTC.HPTC.FTC  
 OPLANT:4.SFRD.HPRO.FRO  
 OPLANT:3.SFRD  
 JOE +3.FPRO F2000  
 FPRO HPRO.FSTA FRO  
 OPLANT:6.SFRCCCR.7.FCR  
 /  
 UDREGN 0  
 OPRAN:0.KD.0  
 UDREGN SIGNA N  
 OPRAN:0A.KSFA.0  
 UDREGN HV+SIGNAF  
 OCL:KSF+70+(KSF+3)+FROINSF  
 OCL:CCSF+6)+FROINSF:(KSF+11)+FCR+(KSF+14)+NSF:NVSF.7)  
 OCL:COBETW+SAZE.7-05A0  
 UDREGN C(J.3-1).C(J.3).C(J.3+1)  
 OCL:C(402+C(J.7)C(J.7)+5-SR(CJJ.7)  
 JA CCF7  
 /  
 SUBROUTINE TIL KOEF.BEREGNING I SEKTION 0 OG 15  
 BASE L00  
 UDREGN. JA 0 /ONSNET FRA HELLTA  
 OPLANT:0.SFTC.HPTC.FTC  
 OPLANT:4.SFRD.HPRO.FRO  
 OPLANT:3.SFRD  
 JOE +3.FPRO F2000  
 FPRO HPRO.FSTA FRO  
 OPLANT:6.SFRCCCR.7.FCR  
 /  
 UDREGN 0  
 OPRAN:0.KD.0  
 UDREGN SIGNA N  
 OPRAN:0A.KSFA.0  
 UDREGN HV+SIGNAF  
 OCL:KSF+70+(KSF+3)+FROINSF  
 OCL:CCSF+6)+FROINSF:(KSF+11)+FCR+(KSF+14)+NSF:NVSF.7)  
 OCL:COBETW+SAZE.7-05A0  
 UDREGN C(J.3-1).C(J.3).C(J.3+1)  
 OCL:C(402+C(J.7)C(J.7)+5-SR(CJJ.7)  
 JA CCF7

/  
 L0SING AF DIFFUSIONSLIGNING  
 /  
 LOES. BASE DX2  
 SETB DX2  
 SETX INDEXS  
 LDX 0.7  
 LDX -17.6 /SEKTIONSANTAL:16  
 FLDR CJI+3.7 /REDUCER MATRICE  
 FDIV CJJ.7  
 FNEO  
 FSTA XX1  
 FFUL CJK+3.7  
 FADDN CJI+3.7  
 FLDR KX1  
 FFUL SLCH.7  
 FADDN SLCH.7  
 JSM L01.6+  
 LDX 17.7 /RETUR HVIS FLERE SEKTIONER  
 LDX -17.6 /SEKTIONSANTAL:16  
 FLDR SLCH.7  
 FDIV CJI.7  
 FSTA PHI.7  
 FFUL CJK+3.7  
 FNEO  
 FADDN SLCH-3.7  
 FLDR PHI.7 /UDREGN FNP  
 FSTA PHIRIN  
 JOE +3.FCLR  
 FPRO PHIRIN  
 FFUL NVSF.7  
 FSTA FNP.7  
 ADDX -1.7  
 JSM L01.6+ /RETUR HVIS FLERE SEKTIONER  
 FLDR SLCH /UDREGN PHI(N) FOR FORSTE SEKTION  
 FDIV CJJ  
 FSTA PHI  
 /  
 ONSNET OG FLVY FNP SON HELLTA  
 BASE FNP  
 SETB FNP  
 SETX N+1  
 LDX 0.7  
 ODPF1X:0CFNP.7+>.SFN  
 ODPF1X:1CFNP.7+>.SFN  
 ODPF1X:2CFNP.7+>.SFN.OVB  
 ODPF1X:3CFNP.7+>.SFN.OVB+2  
 ODPF1X:4CFNP.7+>.SFN.OVB+4  
 ODPF1X:5CFNP.7+>.SFN.OVB+6  
 ODPF1X:6CFNP.7+>.SFN.OVB+8  
 SETX N+10  
 LDX 7.7  
 ODPF1X:0CFNP.7+>.SFN.OVB+12  
 ODPF1X:1CFNP.7+>.SFN.OVB+14  
 ODPF1X:2CFNP.7+>.SFN.OVB+16  
 ODPF1X:3CFNP.7+>.SFN  
 ODPF1X:4CFNP.7+>.SFN  
 ODPF1X:5CFNP.7+>.SFN  
 ODPF1X:6CFNP.7+>.SFN  
 FEXIT

OVB. TRAP6 0 /OVERFLOW AF N/500  
 TRAP6 1  
 TRAP6 2  
 TRAP6 3  
 TRAP6 4  
 TRAP6 5

```

BEREGNING AF KONCENTRATION AF FØRSKINDE NEUTRONER
/
BASE LM1
FPP3. STARTF
      SETB LM1
      SETX INDEX5
      LDX -16.6
      LDX 0.7
FPP3R. FLDA FNP.7          /GRUPPE 1
      FMUL CN1K1
      FADD CN1.7
      FMUL CN1K2
      FSTA CN1.7
      FMUL LM1
      FSTA CNK1
      FLDA FNP.7          /GRUPPE 2
      FMUL CN2K1
      FADD CN2.7
      FMUL CN2K2
      FSTA CN2.7
      FMUL LN2
      FADD CNK1
      FLDA FNP.7          /GRUPPE 3
      FMUL CN3K1
      FADD CN3.7
      FMUL CN3K2
      FSTA CN3.7
      FMUL LN3
      FADD CNK3
      FNEG
      FSTA SLON.7
      JXN FPP3R.6+
      FCMA
      FSTA SLCN
      FSTA SLCN+55
      J8 R10
FIP3EK.

```

DRODTL, F -1. 60  
DRODT, F 0  
/

```

PP22.  STARTF                                /MC,WP,TCU,TPD,TS,F P 00 HIC
       BASE TPL                             /OBSRAETES TIL FPP FORM
       SEVB TPL
       SEVB APD
       OFLONT:0,5FMC, FMC
       OFLONT:3,5FMP, FMP
       OFLONT:2,SFTIN,F300,TPL
       OFLONT:3,SFTIN,F300,TPL+30
       OFLONT:4,SFTIN,F250,FTSA
       OFLONT:0,5FPP,F60,FPR
       OFLONT:6,5FSTIN
       BCAL:~DROOTH,FDT~VCV-ININ
/
/      TEMP:BEREIGNING
/      TIL 1 UPPER PLENUM
/      BCAL:PROK:KXK~FDT~VPL~FKL~XK0
/      BCAL:~FKS~TPL~(CPL+3)~XK0~(TPL+3)
/      TPL~KXK~DROOTHININ
/      SETX INDEXS
/      BCAL:FMP:PROK:KXK~FDT~XK6
/      FLDA DROOTH,FSTA DRODT
/      LDX ~6,0
/      LDX 1,7
/      JSA FPP25                /TEMP. TIL UDGNAG AF U-ROR
/      FLDA DRODTL,FTSA DRODT
/      LDX ~6,0
/      LDX 10,7
/      JSA FPP25                /TEMP. TIL REAKTOR INDL0B
/      BCAL:KXK~XK0~FDT~XK6
/      LDX 16,7
/      JSA FPP25                /TEMP. TIL REAKTOR FOR CORE
/      TPL DROEL TEMP. I U-ROR
/      BCAL:(CPL+17)~F04~FTP:(CPL+20)~F060FTP
/
/      UDREGN APD~4, 5F59/(250~CPP)
/      SEVB APD
/      FLDA:KXK,CPPK,2,FTP
/      FLDA SFDP4
/      FDIY XKS
/      UDREGN:4,,,OV20~10
/      UDREGN APD0= 500/HF0
/      OPOL:KXK,HFKU,2,FTSA
/      FLDA SFDP5
/      FDIY XKS
/      BDFFIX:5,,,OV20~12
/      UDREGN APD6~100/(P0G5~R0F5)
/      OPOL:RUFX,2,FP6
/      BDFFIX:6,,,SFDP6,OV20~14
/      OMSNET T LOWER PLENUM TIL INDEX 0
/      0FX:1:TPL~63,F300,SFTUD,OV20
/      0FX:2:TPL~17,F300,SFTUD,OV20~2
/      0FX:1:TPL~17,F300,SFTUD,OV20~2
/      0FX:2:TPL~25,F300,SFTUD,OV20~4
/      0FX:1:TPL~21,INDEX 1
/      0FX:3:TPL~33,F250,SFTUD
/      0FX:2:TPL~33,F250,SFTUD
/      0FX:1:TPL~33,F250,SFTUD
/      0FX:2:TPL~33,F250,SFTUD
/      JSA TURB

```

TO









Scaled equations, analog diagram, potentiometer list and DFG-tables for the core heat transfer model.

$$\begin{aligned} \left[ \frac{\Delta T_u}{25} \right] &= 1.0996 \left( \left[ \frac{N}{500} \right] - \left[ \frac{Q_u}{500} \right] \right) \\ \left[ \frac{\Delta T_{ca}}{25} \right] &= 6.0478 \left( \left[ \frac{Q_u}{500} \right] - \left[ \frac{Q_c}{500} \right] \right) \end{aligned}$$

$$\left[ \frac{\Delta T_u}{1000} \right]_{n+0.5} = 0.5 \left[ \frac{\Delta T_u}{500} \right]_n + 0.0125 \left[ \frac{\Delta T_u}{25} \right] \quad (\Delta T_u = T_u - 1000)$$

$$\left[ \frac{\Delta T_{ca}}{100} \right]_{n+0.5} = \left[ \frac{\Delta T_{ca}}{100} \right]_n + 0.125 \left[ \frac{\Delta t_{ca}^T}{25} \right] \quad (\Delta T_{ca} = T_{ca} - 300)$$

$$\left[ \frac{T_{\lambda}}{1000} \right] = 0.5 \left[ \frac{\Delta T_u}{1000} \right]_{n+0.5} + 0.05 \left[ \frac{\Delta T_{ca}}{100} \right]_{n+0.5} + 0.1139 \left[ \frac{Q_u}{500} \right] + 0.65$$

$$\left[ \frac{T_u - T_{ca}}{1500} \right] = 0.6667 \left[ \frac{\Delta T_u}{1000} \right]_{n+0.5} - 0.06667 \left[ \frac{\Delta T_{ca}}{100} \right]_{n+0.5} + 0.4667$$

$$\left[ \frac{1}{3} Z_{ugca} \right] = 0.7750 \left[ \frac{2E-6}{\lambda_u} \right] + 0.1519$$

$$\left[ \frac{Q_u}{500} \right] = \frac{1}{\left[ \frac{1}{3} z_{ugca} \right]} \left[ \frac{T_u - T_{ca}}{1500} \right]$$

$$\left[ \frac{T_{ca} - T_c}{100} \right] = \left[ \frac{\Delta T_{ca}}{100} \right]_{n+0.5} - \left[ \frac{\Delta T_c}{100} \right] - 0.5$$

$$\left[ \frac{Q_{cl}}{500} \right] = 2.0584 \left[ \frac{W_c}{15000} \right]^{0.8} \left[ \frac{T_{ca} - T_c}{100} \right]$$

$$\left[ \frac{Q_{c2}}{500} \right] = 0.8785 \left[ \frac{T_{ca} - T_{pa}}{5} \right]^2$$

$$\left[\frac{\Delta T_c}{50}\right]_{n+1}^j = \left[\frac{\Delta T_c}{50}\right]_{n+1}^{j-1} + \frac{0.2}{\frac{W}{C} \left[\frac{15000}{1000}\right]} \left( 0.3333 \left[\frac{500}{1000}\right] - 0.6747 \left[\frac{P_f}{1000}\right] \left[\frac{A_c}{10}\right]_{n+1}^j \right)$$

(melting point: 204°C)

$$\left[ \frac{\Delta T}{10} \right]_{n+1}^j = b \left( \left[ \frac{\Delta T}{50} \right]_{n+1}^j - \left[ \frac{\Delta T}{50} \right]_n^j \right)$$

01	15651	ME	15741
02	15652	ME	15742
03	15653	ME	15743
04	15654	ME	15744
05	15655	ME	15745
06	15656	ME	15746
07	15657	ME	15747
08	15658	ME	15748
09	15659	ME	15749
10	15660	ME	15750
11	15661	ME	15751
12	15662	ME	15752
13	15663	ME	15753
14	15664	ME	15754
15	15665	ME	15755
16	15666	ME	15756
17	15667	ME	15757
18	15668	ME	15758
19	15669	ME	15759
20	15670	ME	15760
21	15671	ME	15761
22	15672	ME	15762
23	15673	ME	15763
24	15674	ME	15764
25	15675	ME	15765
26	15676	ME	15766
27	15677	ME	15767
28	15678	ME	15768
29	15679	ME	15769
30	15680	ME	15770
31	15681	ME	15771
32	15682	ME	15772
33	15683	ME	15773
34	15684	ME	15774
35	15685	ME	15775
36	15686	ME	15776
37	15687	ME	15777
38	15688	ME	15778
39	15689	ME	15779
40	15690	ME	15780
41	15691	ME	15781
42	15692	ME	15782
43	15693	ME	15783
44	15694	ME	15784
45	15695	ME	15785
46	15696	ME	15786
47	15697	ME	15787
48	15698	ME	15788
49	15699	ME	15789
50	15700	ME	15790
51	15701	ME	15791
52	15702	ME	15792
53	15703	ME	15793
54	15704	ME	15794
55	15705	ME	15795
56	15706	ME	15796
57	15707	ME	15797
58	15708	ME	15798
59	15709	ME	15799
60	15710	ME	15800
61	15711	ME	15801
62	15712	ME	15802
63	15713	ME	15803
64	15714	ME	15804
65	15715	ME	15805
66	15716	ME	15806
67	15717	ME	15807
68	15718	ME	15808
69	15719	ME	15809
70	15720	ME	15810
71	15721	ME	15811
72	15722	ME	15812
73	15723	ME	15813
74	15724	ME	15814
75	15725	ME	15815
76	15726	ME	15816
77	15727	ME	15817
78	15728	ME	15818
79	15729	ME	15819
80	15730	ME	15820
81	15731	ME	15821
82	15732	ME	15822
83	15733	ME	15823
84	15734	ME	15824
85	15735	ME	15825
86	15736	ME	15826
87	15737	ME	15827
88	15738	ME	15828
89	15739	ME	15829
90	15740	ME	15830
91	15741	ME	15831
92	15742	ME	15832
93	15743	ME	15833
94	15744	ME	15834
95	15745	ME	15835
96	15746	ME	15836
97	15747	ME	15837
98	15748	ME	15838
99	15749	ME	15839
00	15750	ME	15840

$$\left[ \frac{\Delta T_c}{100} \right] = 0.25 \left( \left[ \frac{\Delta T_c}{50} \right]_{n+1}^{j-1} + \left[ \frac{\Delta T_c}{50} \right]_{n+1}^j - 0.2 \left[ \frac{\Delta T_c}{10} \right]_{n+1}^j - 0.2 \right)$$

(zeropoint: 250°C)

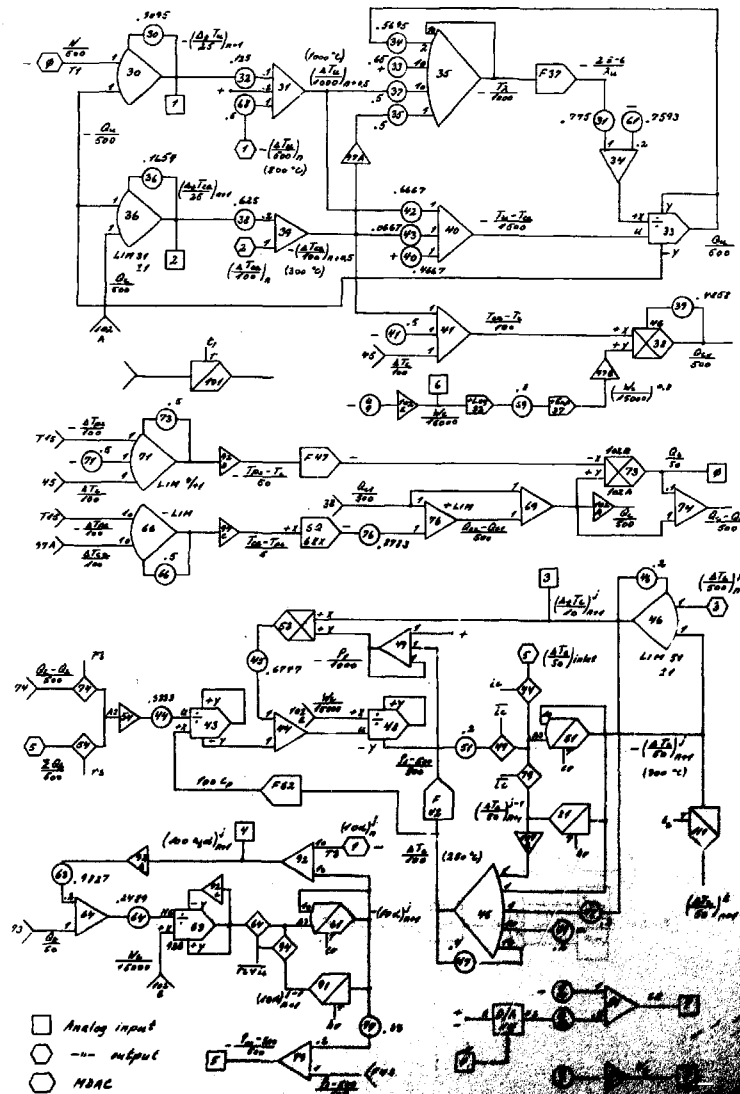
$$\left[ \frac{Q_b}{50} \right] = \left[ \frac{Q_c}{500} \right] * F \left( \left[ \frac{T_{ps} - T_c}{50} \right] \right)$$

$$[10a]_{n+1}^j = [10a]_{n+1}^{j-1} + \frac{0.2489}{\left[ \frac{W_c}{15000} \right]} \left( \left[ \frac{Q_b}{50} \right] - 0.1965 [100\Delta_t a]_{n+1}^j \right)$$

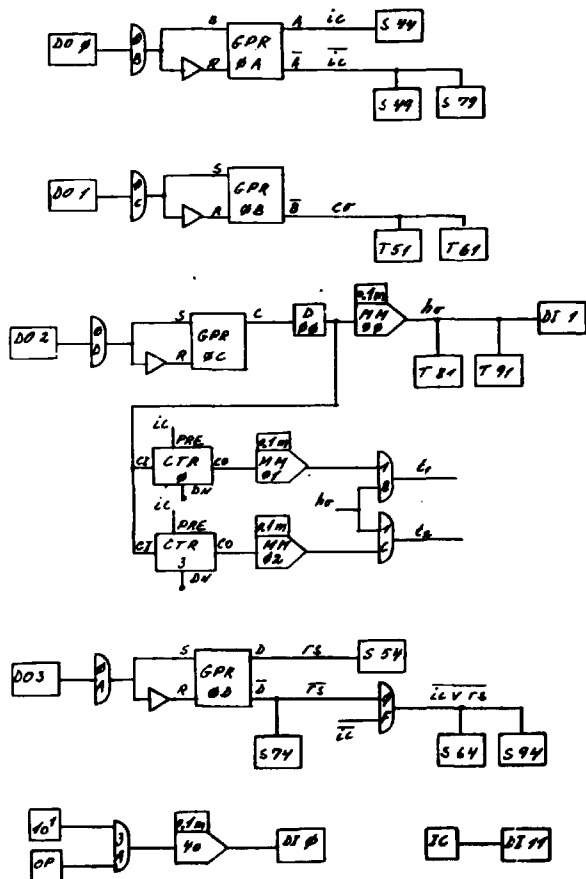
$$[100\Delta_t a]_{n+1}^j = 10 \left( [10a]_{n+1}^j - [10a]_n^j \right)$$

$$\left[ \frac{\rho_m - 500}{500} \right] = \left[ \frac{\rho_f - 500}{500} \right] - 0.128 [10a]_{n+1}^j$$

Analog computing diagram for the core heat transfer



# Analog logic diagram.



## Potentiometer list.

$$P30 = \frac{C_u}{\Delta t} \frac{SF N}{SF A_t T_u} = \frac{1.819 \cdot 25}{0.1 \cdot 500} = 0.9095$$

$$P32 = \frac{1}{2} \frac{SF \Delta T_u}{SF A_t T_u} \cdot 10 = \frac{1}{2} \cdot \frac{25}{1000} \cdot 10 = 0.125$$

$$P68 = 0.5$$

$$P36 = \frac{C_{ca}}{\Delta t} \frac{SF Q_u}{SF A_t T_{ca}} = \frac{0.3307 \cdot 25}{0.1 \cdot 500} = 0.1654$$

$$P38 = \frac{1}{2} \frac{SF \Delta T_{ca}}{SF A_t T_{ca}} \cdot 5 = \frac{1}{2} \cdot \frac{25}{100} \cdot 5 = 0.625$$

$$P33 = \frac{1}{2} (T_{uo} + T_{cao}) (SF T_{\lambda}) = \frac{1}{2} \cdot \frac{1000 + 300}{1000} = 0.65$$

$$P37 = \frac{1}{2} \frac{SF T_{\lambda}}{SF T_u} = 0.5$$

$$P35 = \frac{1}{2} \frac{SF T_{\lambda}}{SF T_{ca}} \cdot 10 = 0.5$$

$$P34 = \frac{1}{2} Z_{gca} \frac{SF T_{\lambda}}{SF Q_u} \cdot 5 = \frac{1}{2} \cdot 0.4556 \cdot \frac{5}{2} = 0.5695$$

$$P61 = 5 Z_{gca} \cdot (SF Z_{ugca}) = 5 \cdot 0.4556 \cdot \frac{1}{3} = 0.7593$$

$$P31 = K_u \frac{SF Z_{ugca}}{SF 17 \lambda_u} = \frac{4.65E-6}{3 \cdot 2E-6} = 0.775$$

$$P40 = (T_{uo} - T_{cao}) \cdot SF (T_u - T_{ca}) = \frac{1000 - 300}{1500} = 0.4667$$

$$P42 = \frac{SF (T_u - T_{ca})}{SF \Delta T_u} = \frac{1000}{1500} = 0.6667$$

$$P43 = \frac{SF (T_u - T_{ca})}{SF \Delta T_{ca}} = \frac{100}{1500} = 0.0667$$

$$P41 = (T_{cao} - T_{co}) \cdot SF T_c = \frac{300 - 250}{100} = 0.5$$

$$P39 = \frac{1}{\left( \frac{0.023E-3}{D_{ec} 0.2} \right)^{0.8} \cdot H_c \cdot SF \left( \frac{1}{A_c = SF W_c} \right)} \cdot \frac{SF Q_{c1}}{SF (T_{ca} - T_{co})}$$

$$= \frac{1}{\left( \frac{0.023E-3}{0.01435 0.2} \right)^{0.8} \cdot 280.9 \cdot \left( \frac{15000}{1.68} \right)^{0.8} \cdot 0.92E-3 \cdot \frac{100}{100}} = 0.4888$$

$$P69 = 0.8$$

$$P73 = \frac{SF \Delta T_{ps}}{SF (T_{ps} - T_c)} = \frac{50}{100} = 0.5$$

$$P71 = (T_{pso} - T_{co}) \cdot SF(T_{ps} - T_c) \cdot P73 = \frac{300-250}{50 \cdot 2}$$

$$P66 = \frac{SF \Delta T_{ps}}{SF (T_{ca} - T_{ps})} 10 = \frac{5}{100} \cdot 10 = 0.5$$

$$P76 = 1.473E-3 \cdot 0_{ca} \cdot \exp\left(\frac{P}{43.4}\right) \cdot \frac{5^2}{500} = 0.8782$$

$$P44 = \frac{SF W_c \cdot SF C_p}{SF Q} = \frac{500 \cdot 100}{15000} = 0.3333$$

$$P45 = \frac{V_c \cdot SF W_c}{\Delta t \cdot SF \rho_f \cdot SF \Delta T_c} = \frac{1.012 \cdot 1000 \cdot 10}{0.1 \cdot 15000} = 0.6747$$

$$P51 = 10 \cdot SF \Delta T_c = \frac{10}{50} = 0.2$$

$$P46 = \frac{SF \Delta T_c}{SF \Delta T_c} = \frac{10}{50} = 0.2$$

$$P47 = 2 \cdot \frac{SF \Delta T_c}{SF T_c} \cdot \frac{1}{10} = 0.2 \cdot \frac{100}{50} = 0.4$$

$$P48 = \frac{1}{2} \cdot \frac{SF T_c}{SF \Delta T_c} \cdot 10 \cdot P47 = \frac{1}{2} \cdot \frac{10}{100} \cdot 4 = 0.2$$

$$P49 = (\Delta T_{co} - T_{co}) \cdot SF T_c \cdot P47 = (300-250) \cdot \frac{0.4}{100} = 0.2$$

$$P64 = \frac{\rho_f}{n_{fg} \rho_{gs}} \frac{SF W_c}{SF Q_k} 10 = \frac{725}{97.1} \cdot \frac{50 \cdot 10}{15000} = 0.2489$$

$$P63 = \frac{V_c}{\Delta t n_{fg} \rho_{gs}} \frac{SF Q_k}{SF \Delta T_c} = \frac{1.012}{0.1} \cdot 97.1 \cdot \frac{5}{50 \cdot 100} = 0.9827$$

$$P74 = (\rho_f - \rho_{gs}) \frac{SF \rho_m}{SF \alpha} 5 = 630 \cdot \frac{5}{500 \cdot 10} = 0.63$$

$$Q7 = W_b$$

$$Q1 = \frac{W_c}{15000} = 0.8460$$

Q12: ACh-position

Q14: ACh-position

# DFG-tables.

F32:  $[100 C_p]$  MJ/kg °C at 150 bar.

T °C	$x = \frac{\Delta T_c}{100}$	$C_p$	$Y = [100 C_p]$
250	0.00	0.00473	0.473
270	0.20	0.00495	0.495
290	0.40	0.00526	0.526
300	0.50	0.00548	0.548
310	0.60	0.00579	0.579
320	0.70	0.00621	0.621
330	0.80	0.00687	0.687
335	0.85	0.00737	0.737
340	0.90	0.00809	0.809
345	0.95	0.00905	0.905
305	1.00	0.01000	1.000

extension for 150 bar

F42:  $[(\rho_f - 500)/500]$  kg/m<sup>3</sup> at 150 bar

T °C	$\frac{\Delta T_c}{100}$	$\rho_f$ kg/m <sup>3</sup>	$\frac{\rho_f - 500}{500}$ kg/m <sup>3</sup>
250	0.00	811.4	0.623
260	0.10	796.6	0.593
270	0.20	780.8	0.562
280	0.30	763.9	0.528
290	0.40	745.7	0.491
300	0.50	725.7	0.451
310	0.60	703.6	0.407
320	0.70	678.6	0.357
330	0.80	649.3	0.299
340	0.90	618.2	0.238
350	1.00	578.6	0.157

$$F37: - \left[ 2E-6/\lambda_u \right] m^{\circ}C/m^2$$

T °C	$\lambda = \frac{T}{1000}$	$\lambda_u W/m^{\circ}C$	$\frac{2E-6}{\lambda_u}$
0	0.00	8.40	0.238
100	0.10	7.00	0.286
200	0.20	5.95	0.336
300	0.30	5.17	0.387
400	0.40	4.60	0.435
500	0.50	4.13	0.484
600	0.60	3.77	0.531
700	0.70	3.46	0.578
800	0.80	3.21	0.623
900	0.90	2.98	0.671
1000	1.00	2.78	0.719

$$F47: \left[ 10 \cdot \frac{Q_b}{Q_c} \right]$$

$\frac{T_{sa}-T_c}{50}$	$10 \frac{Q_b}{Q_c}$
0.00	1.000
0.08	0.870
0.12	0.770
0.16	0.630
0.20	0.500
0.30	0.300
0.40	0.180
0.50	0.100
0.60	0.050
0.80	0.010
1.00	0.000

# APPENDIX C

Scaled equations, analog diagram, potentiometer list, DFG-tables and parameter tables for the steam generator model.

## Scaled equations.

$$\left[ \frac{p_o}{50} \right] = \left[ \frac{T_{p1,2}}{50} \right] - \left[ \frac{\Delta T_{po}}{50} \right]$$

$$\left[ \frac{\Delta T_{po}}{50} \right] = 0.330 \left( \left[ \frac{Q_p}{250 C_{pp}} \right] - \left[ \frac{W_p}{5000} \right] \left[ \frac{\Delta T_{po}}{50} \right] \right)$$

$$\left[ \frac{T_p}{50} \right] = 0.41 \left[ \frac{T_{p1}}{50} \right] + 0.59 \left[ \frac{T_{po}}{50} \right]$$

$$\left[ \frac{T_{r1}}{50} \right] = 4.036 \left[ \frac{Q_p}{2000} \right] - 5.017 \left( \left[ \frac{T_{r1}}{50} \right] - \left[ \frac{T_{r2}}{50} \right] \right)$$

$$\left[ \frac{T_{r2}}{50} \right] = 5.017 \left( \left[ \frac{T_{r1}}{50} \right] - \left[ \frac{T_{r2}}{50} \right] \right) - 2.018 \left[ \frac{Q_s}{1000} \right]$$

$$\left[ \frac{Q_p}{2000} \right] = 0.8725 \left[ \frac{W_p}{5000} \right]^{0.8} \left[ \frac{T_p - T_{r1}}{10} \right]$$

$$\left[ \frac{Q_s}{1000} \right] = \left[ \frac{T_{r2} - T_{ss}}{4.849} \right]^2$$

$$\left[ \frac{Q_k}{1000} \right] = \left[ \frac{Q_s}{1000} \right] - 0.260 \left[ \frac{W_s}{5000} \right] \left[ \frac{T_{ss} - T_d}{10} \right]$$

$$\left[ 10 \dot{U} \right] = \left[ \frac{5.80}{h_{gs}} \right] \left[ \frac{Q_k}{1000} \right] - 5.80 \left[ \frac{W_g}{1000} \right] - 1.14 \left[ \frac{p_s}{2} \right]$$

$$\left[ \frac{W_f}{5000} \right] = \left[ \frac{W_g}{5000} \right] - 0.2 \left[ \frac{W_g}{1000} \right] + 0.756 \left[ 10 \dot{U} \right] + 0.0208 \left[ \frac{p_s}{2} \right]$$

$$\left[ \frac{W_g}{1000} \right] = 0.75 \left[ \frac{W_f}{5000} \right] \left[ \frac{a}{1-a} \right] \left[ 10 \frac{p_{gs}}{p_{fs}} \right]$$

$$[a] = [U] (2.33 - 1.74 [U])$$

$$[\dot{a}_r] = [a] - [a_r]$$

$$\left[ \frac{\dot{p}_s}{2} \right] = 6.66 \left( \left[ \frac{W}{1000} \right] - \left[ \frac{W_1}{1000} \right] \right) - 2.778 \left[ \frac{a_s}{2} \right]$$



$$\begin{bmatrix} \dot{W}_b \\ 5000 \end{bmatrix} = \begin{bmatrix} \dot{W}_f \\ 5000 \end{bmatrix} + 0.0112 \begin{bmatrix} \dot{P}_s \\ 2 \end{bmatrix} + 1.89 \begin{bmatrix} \dot{a}_r \end{bmatrix}$$

$$\begin{bmatrix} \dot{T}_b \\ 5 \end{bmatrix} = 0.0703 \begin{bmatrix} \dot{W}_b \\ 5000 \end{bmatrix} \begin{bmatrix} T_{sa} - T_b \\ 10 \end{bmatrix} - 0.1333 \begin{bmatrix} \dot{W}_i \\ 1000 \end{bmatrix} \begin{bmatrix} T_b - T_i \\ 100 \end{bmatrix}$$

$$\begin{bmatrix} \dot{T}_c \\ 57 \end{bmatrix} = 0.1911 \begin{bmatrix} \dot{W}_s \\ 5000 \end{bmatrix} \begin{bmatrix} T_b - T_c \\ 10 \end{bmatrix}$$

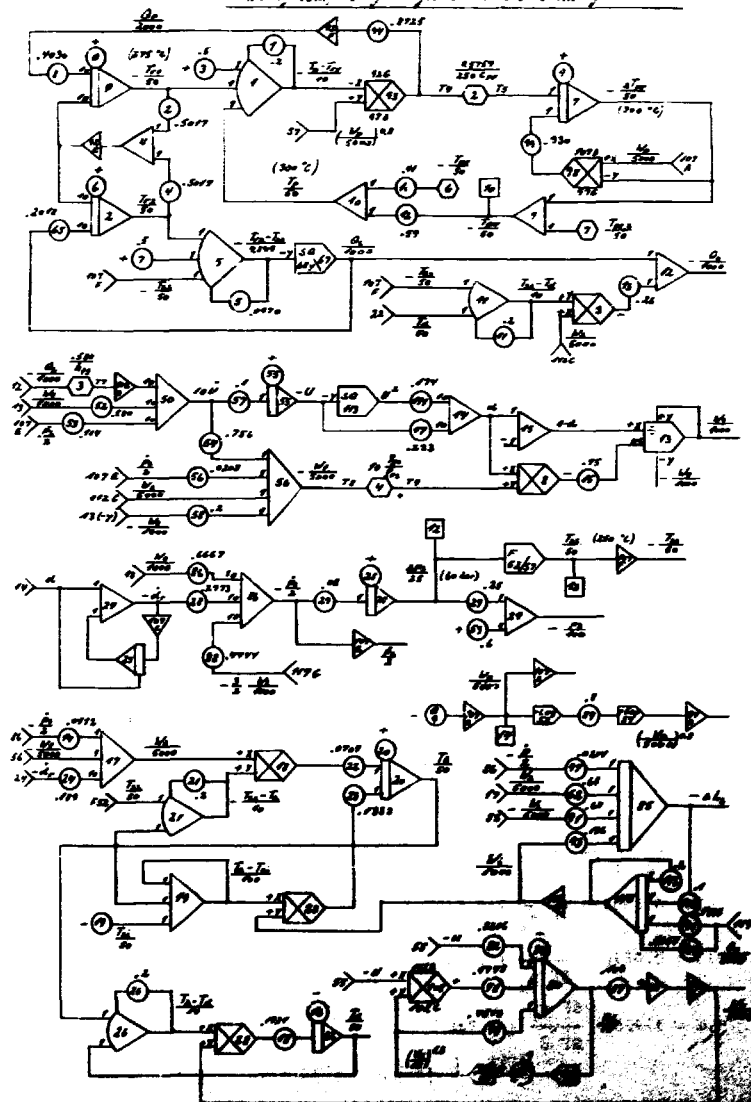
$$\begin{bmatrix} \dot{\Delta P} \\ 100 \rho_{fs} \end{bmatrix} = (0.5464 + 0.2152 [U]) \begin{bmatrix} \dot{V}_d \\ 10 \end{bmatrix} \mu.8$$

$$\begin{bmatrix} \dot{V}_d \\ 10 \end{bmatrix} = 0.8206 [U] - 0.826 \begin{bmatrix} \dot{\Delta P} \\ 100 \rho_{fs} \end{bmatrix}$$

$$\begin{bmatrix} \dot{W}_s \\ 5000 \end{bmatrix} = 1.03 \begin{bmatrix} \dot{V}_d \\ 10 \end{bmatrix}$$

$$[U] = 0.680 \left( \begin{bmatrix} \dot{W}_b \\ 5000 \end{bmatrix} - \begin{bmatrix} \dot{W}_s \\ 5000 \end{bmatrix} \right) + 0.136 \begin{bmatrix} \dot{W}_i \\ 1000 \end{bmatrix} - 0.0204 \begin{bmatrix} \dot{P}_s \\ 2 \end{bmatrix}$$

Analogue computing diagram for the steam generator



Potentiometer list

$$P1 = \frac{SF T_{r1}}{SF (T_p - T_{r1})} = \frac{10}{50} = 0.2$$

$$P2 = \frac{1}{10} \cdot \frac{1}{C_r L_c} \cdot \frac{\lambda_r}{\Delta r} 2L_c 0_r = 0.1 \cdot 0.1009 \cdot 49.71 = 0.5017$$

$$P3 = SF T_{r1} \cdot (\text{zerop. } T_p - \text{zerop. } T_{r1}) = \frac{300-275}{50} = 0.5$$

$$P4 = P2 = 0.5017$$

$$P5 = \frac{SF T_{r2}}{SF (T_{ss} - T_{r2})} = \frac{4.849}{50} = 0.0970$$

$$P7 = SF T_{r2} \cdot (\text{zerop. } T_{r2} - \text{zerop. } T_{ss}) = \frac{275-250}{50} = 0.5$$

$$P8 = \frac{1}{10} \cdot \frac{1}{C_r L_c} \cdot \frac{SF T_{r1}}{SF 0_p} = 0.1 \cdot 0.1009 \cdot \frac{2000}{50} = 0.4036$$

$$P6s = \frac{1}{10} \cdot \frac{1}{C_r L_c} \cdot \frac{SF T_{r2}}{SF 0_s} = 0.1 \cdot 0.1009 \cdot \frac{1000}{50} = 0.2018$$

$$P10 = a_p = 0.41$$

$$P12 = 1 - a_p = 0.59$$

$$P11 = \frac{SF T_d}{SF (T_{ss} - T_d)} = \frac{10}{50} = 0.2$$

$$P13 = \frac{SF Q_k}{SF W_a \cdot SF (T_{ss} - T_d)} = 0.0052 \cdot \frac{5000 \cdot 10}{1000} = 0.26$$

$$P94 = \frac{0.023E-3}{D_{ep} 0_{..}} 0_p 2L_c \left( \frac{SF W_b}{A_p} \right)^{0.8} \frac{SF Q_p}{SF (T_p - T_{r1})} \\ = 0.1917 \cdot 5000^{0.8} \cdot \frac{10}{2007} = 0.8725$$

$$P99 = \frac{1}{V_p P_f} \cdot \frac{1}{SF W_p} = 0.560E-4 \cdot 5000 = 0.330$$

$$P52 = 0.580E-3 \cdot \frac{1}{SF W_g} = 0.580E-3 \cdot 10 \cdot 1000 = 0.580$$

$$P53 = 0.0570 \cdot \frac{1}{SF P_s} = 0.0570 \cdot 2 = 0.114$$

$$P54 = 37800 \cdot \frac{SF W_f}{SF \eta} = 0.756$$

$$P56 = 52 \cdot \frac{SF W_f}{SF P_s} = 0.0208$$

$$P57 = \frac{SF U}{SF \dot{U}} = 0.1$$

$$P58 = \frac{SF W_f}{SF W_g} = \frac{1000}{5000} = 0.2$$

$$P17 = 0.233$$

$$P111 = 0.174$$

$$P15 = \frac{1.5 \cdot SF W_g}{SF W_f \cdot SF (P_{gs} / \rho_{fs})} = \frac{1.5 \cdot 5000}{1000 \cdot 10} = 0.75$$

$$P27 = \frac{SF \Delta P_b}{SF P_s} = \frac{2}{25} = 0.08$$

$$P28 = \frac{1}{10} \cdot \frac{V_r P_{gs}}{75} \cdot \frac{SF P_s}{SF \dot{Q}_r} = 0.1 \cdot \frac{416}{75} \cdot 0.5 = 0.2773$$

$$P29 = \frac{SF P_s}{SF \Delta P_b} = \frac{25}{100} = 0.25$$

$$P59 = SF P_s \cdot \text{zerop. } P_s = 0.01 \cdot 60 = 0.6$$

$$P86 = \frac{1}{10} \cdot \frac{1}{75} \cdot \frac{SF P_s}{SF W_g} = \frac{1}{750} \cdot \frac{1000}{2} = 0.6667$$

$$P88 = \frac{1}{10} \cdot \frac{1}{75} \cdot \frac{SF P_s}{SF W_1} = \frac{1}{750} \cdot \frac{2000}{3.2} = 0.4444$$

$$P14 = C1 \cdot \frac{SF W_b}{SF P_s} = 28 \cdot \frac{2}{5000} = 0.0112$$

$$P19 = \frac{250 T_{s1}}{SF T_{s1}} = \frac{24}{50} = 0.48$$

$$P21 = \frac{SF T_{ss}}{SF (T_{ss} - T_b)} = \frac{10}{50} = 0.2$$

$$P22 = \frac{1}{V_{b1} \rho_{fs}} \cdot \frac{SF T_b}{SF W_a \cdot SF (T_{ss} - T_b)} = 0.709E-4 \cdot \frac{5000 \cdot 10}{50} = 0.0709$$

$$P23 = \frac{1}{V_{b1} \rho_{fs}} \cdot \frac{C_{pm} SF T_b}{C_{pm} SF W_1 \cdot SF (T_b - T_{s1})} = 0.94 \cdot 0.709E-4 \cdot \frac{2000 \cdot 100}{50} = 0.0094$$

$$P24 = \frac{V_r P_{fs}}{10} \cdot \frac{SF W_b}{SF \dot{Q}_r} = 945 \cdot \frac{1}{5000} = 0.189$$

$$P18 = \frac{1}{V_d \rho_{fs}} \cdot \frac{SF T_d}{SF W_a \cdot SF (T_b - T_d)} = 1.921E-4 \cdot \frac{5000 \cdot 10}{50} = 0.1921$$

$$P26 = \frac{SF T_b}{SF(T_b - T_d)} = \frac{10}{50} = 0.2$$

$$P64 = 0.6$$

$$P61 = 0.9$$

$$P62 = \frac{z V_g / A_s}{L A_d / A_s} \frac{SF v_d}{SF U} = 0.0826 \cdot 99.34 \cdot 0.1 = 0.8206$$

$$P75 = 0.2152 \cdot 0.826 = 0.1778$$

$$P73 = 0.5464 \cdot 0.826 = 0.4513$$

$$P87 = \frac{1}{10} \cdot A_d \rho_{fs} \frac{SF W_s}{SF v_d} = \frac{515}{10} \cdot \frac{10}{5000} = 0.103$$

$$P = \frac{1}{A_d \rho_{fs}} \frac{SF \Delta L_b}{SF W_b} = 0.136E-3 \cdot 5000 = 0.68$$

$$P = \frac{1}{A_b \rho_{fs}} \frac{SF \Delta L_b}{SF W_s} = 0.136E-3 \cdot 5000 = 0.68$$

$$P = \frac{1}{A_b \rho_{fs}} \frac{SF \Delta L_b}{SF W_i} = 0.136E-3 \cdot \frac{2000}{3} = 0.0907$$

$$P = \frac{EV}{A_b \rho_{fs}} \frac{dp_{fs}}{dp_s} \frac{SF \Delta L_b}{SF p_s} = 0.136E-3 \cdot 75 \cdot 2 = 0.0204$$

IC-value potentiometers:

$$P4: \frac{T_{F1}}{50}, \text{ zeropoint: } 275^\circ \text{C}$$

$$P6: \frac{T_{F2}}{50}, \quad " \quad : 275^\circ \text{C}$$

$$P9: \frac{\Delta T_{P0}}{50}, \quad " \quad : 300^\circ \text{C}$$

$$P39: \quad , \quad " \quad : 0$$

$$P20: \frac{T_L}{50}, \quad " \quad : 250^\circ \text{C}$$

$$P16: \frac{T_G}{50}, \quad " \quad : 250^\circ \text{C}$$

$$P15: \frac{\Delta P_0}{75}, \quad " \quad : 60 \text{ bar}$$

# DFG table

F 52/57:  $(T_{ss}/50)^\circ \text{C}$

p bar	T °C	Δp bar	x	ΔT °C	y
35.0	242.5	-25.0	-1.000	-7.5	-0.150
37.5	246.5	-22.5	-0.900	-3.5	-0.070
40.0	250.3	-20.0	-0.800	0.3	0.006
42.5	254.0	-17.5	-0.700	4.0	0.080
45.0	257.4	-15.0	-0.600	7.4	0.148
47.5	260.7	-12.5	-0.500	10.7	0.214
50.0	263.9	-10.0	-0.400	13.9	0.278
52.5	267.0	-7.5	-0.300	17.0	0.340
55.0	269.9	-5.0	-0.200	19.9	0.398
57.5	272.8	-2.5	-0.100	22.8	0.456
60.0	275.6	0.0	0.000	25.6	0.512
62.5	278.2	2.5	0.100	28.2	0.564
65.0	280.8	5.0	0.200	30.8	0.616
67.5	283.3	7.5	0.300	33.3	0.666
70.0	285.8	10.0	0.400	35.8	0.716
72.5	288.2	12.5	0.500	38.2	0.764
75.0	290.5	15.0	0.600	40.5	0.810
77.5	292.8	17.5	0.700	43.8	0.856
80.0	295.0	20.0	0.800	45.0	0.900
82.5	297.2	22.5	0.900	47.2	0.944
85.0	299.2	25.0	1.000	49.2	0.984

Table C1

T °C	P bar	$h_{fg}$ kJ/kg	$\rho_{fs}$ kg/m <sup>3</sup>	$\rho_{gs}$ kg/m <sup>3</sup>	$\frac{dh_{fs}}{dp_s}$ kJ/kg	$\frac{dh_{gs}}{dp_s}$ kJ/kg	$\frac{dp_{fs}}{dp_s}$ kg/m <sup>3</sup>	$\frac{dp_{gs}}{dp_s}$ kg/m <sup>3</sup>	$\frac{10^6 ds}{dp_s}$ bar	A kJ/m <sup>3</sup> bar	B kJ/m <sup>3</sup> bar	C kJ/m <sup>3</sup> bar
260	40.1	1660	784	23.7	0.5	-0.85	-2.05	0.54	0.303	876	5096	-20.1
270	55.1	1605	769	28.1	5.9	-1.10	-1.93	0.55	0.366	851	4531	-30.9
280	64.2	1540	751	33.2	5.4	-1.27	-1.82	0.57	0.442	836	4055	-42.2
290	74.5	1475	732	39.2	5.0	-1.41	-1.75	0.60	0.535	830	3660	-55.3
300	85.9	1400	712	46.2	4.6	-1.54	-1.70	0.63	0.649	811	3275	-71.1

$$A = \rho_{gs} \frac{dh_{gs}}{dp_s} + h_{fg} \frac{d\rho_{gs}}{dp_s}$$

$$B = \rho_{fs} \frac{dh_{fs}}{dp_s}$$

$$C = \rho_{gs} \frac{dh_{gs}}{dp_s}$$

Table C2

Load W	P bar	$V_g$ m <sup>3</sup>	$\alpha$	U	F <sub>a</sub>	D kg/bar	E kg/bar	C1 kg/bar	C2 kg/bar	$\Sigma R_{ax}$ m	W <sub>g</sub> kg/s	$\tau_r$ sec.
115	49.2	25.6	0.739	0.490	1.45	91.2	-39.9	27.5	73.1	39.1	547	0.42
100	53.4	23.4	0.699	0.448	1.56	94.7	-43.3	27.9	73.8	34.4	475	0.50
90	56.4	21.7	0.673	0.416	1.62	97.2	-46.6	28.0	74.1	31.5	428	0.56
75	60.0	19.1	0.623	0.367	1.70	98.1	-51.2	27.4	73.8	27.5	356	0.68
65	63.9	17.45	0.583	0.335	1.73	98.0	-53.7	27.0	73.8	25.0	309	0.78
50	66.2	14.85	0.514	0.285	1.81	100.2	-58.2	27.6	74.9	21.7	237	0.98
40	71.4	12.70	0.461	0.243	1.90	102.8	-62.5	28.5	76	19.5	188	1.16
25	78.1	9.41	0.366	0.180	2.03	107.6	-68.8	30.5	78.4	16.5	119	1.55

$$V = \frac{1}{\rho_{fg}} (\alpha V_g + \beta V_f - 100 V_s)$$

$$E = V_g \frac{dp_{gs}}{dp_s} + V_f \frac{dp_{fs}}{dp_s}$$

$$C1 = \frac{1}{\rho_{fg}} \left( \rho_{fs} \frac{dh_{fs}}{dp_s} (V_g + V_f (1 - \alpha_r)) + (V_e + \alpha_r V_r) \left( \rho_{gs} \frac{dh_{gs}}{dp_s} - 100 \right) \right)$$

$$C2 = C1 + \frac{d\rho_{gs}}{dp_s} (V_e + \alpha_r V_r)$$

# APPENDIX D

Scaled equations, analog diagram, potentiometer list, and DFG-table for the turbine-reheater model.

## Scaled equations

$$\left[ \frac{\dot{p}_h}{100} \right] = 4.700 \left[ \frac{\dot{q}_v}{2000} \right] - 0.13 \left[ \frac{p_h}{100} \right]$$

$$\left[ \frac{\dot{p}_v}{20} \right] = 4.4730 (1-a_1) \left[ \frac{p_h}{100} \right] - 2.94 \left[ \frac{p_l}{20} \right]$$

$$\left[ \frac{\dot{q}_v}{2000} \right] = 1.530 \left[ \dot{q}_v \right] \left[ \frac{p_v}{100} \right] \left[ y_v \right]$$

$$\left[ \frac{\dot{q}_v}{2000} \right] = 0.9346 (1-a_2) \left[ \frac{p_h}{100} \right]$$

$$\left[ \frac{\dot{t}_{t2}}{50} \right] = 0.6610 \left[ \frac{t_{t2} - t_{t1}}{50} \right] - 0.1212 \left[ \frac{q_r}{200} \right]$$

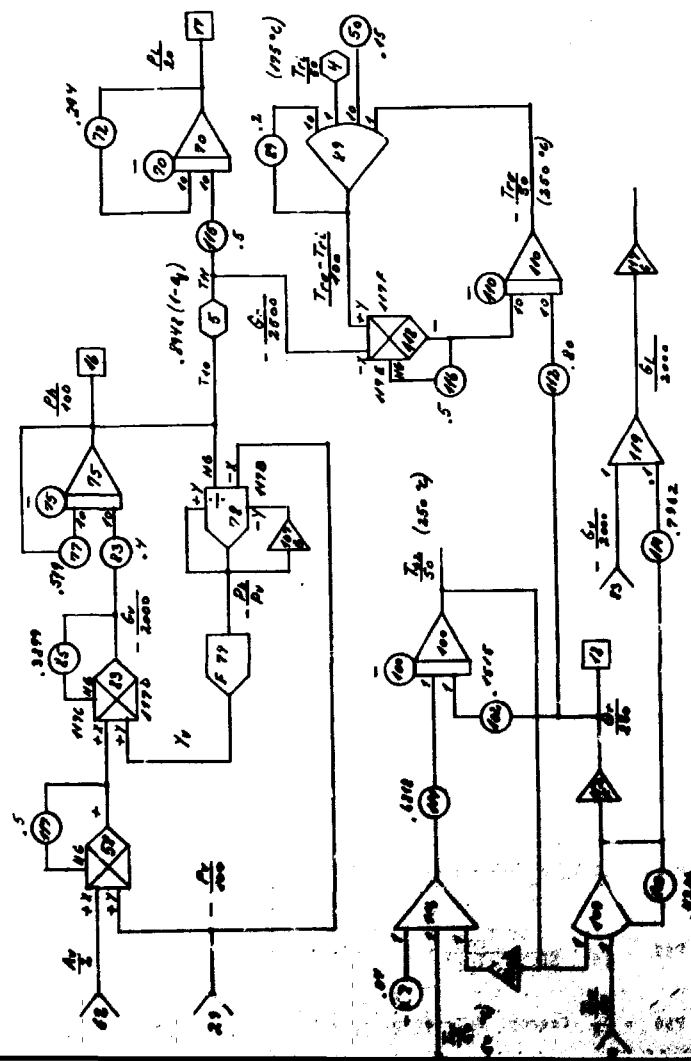
$$\left[ \frac{t_{t2} - t_{t1}}{50} \right] = \left[ \frac{t_{t2}}{50} \right] - \left[ \frac{t_{t1}}{50} \right] - 0.04$$

$$\left[ \frac{q_r}{20} \right] = 1.50 \left[ \frac{t_{t2} - t_{t1}}{50} \right]$$

$$\left[ \frac{\dot{q}_r}{200} \right] = 0.4 \left[ \frac{q_r}{200} \right] - 10 \left[ \frac{q_r}{2500} \right] \left[ \frac{t_{ro} - t_{ri}}{100} \right]$$

$$\left[ \frac{\dot{q}_r}{200} \right] = \left[ \frac{q_r}{200} \right] + 0.0037 \left[ \frac{q_r}{200} \right]$$

## Analog computing diagram for the turbine-reheater.



Potentiometer list

$$P117 = 0.5$$

$$P85 = \frac{1}{k_v} \frac{SF P_v}{SF G_v} = \frac{2000}{51.3 \cdot 100} = 0.3899$$

$$P83 = \frac{1}{10} \cdot \frac{1}{v_h} \frac{d\rho_g}{d\rho} \frac{SF P_h}{SF G_v} = 0.1 \cdot \frac{1}{10 \cdot 0.5} \cdot \frac{2000}{100} = 0.4$$

$$P77 = \frac{1}{10} \cdot \frac{1}{v_h} \frac{d\rho_g}{d\rho} k_h = 0.1 \cdot \frac{1}{10 \cdot 0.5} \cdot 25.95 = 0.519$$

$$P72 = \frac{1}{10} \cdot \frac{1}{v_l} \frac{d\rho_g}{d\rho} k_l = 0.1 \cdot \frac{1}{50 \cdot 0.5} \cdot 73.5 = 0.294$$

$$P115 = \frac{1}{10} \cdot \frac{1}{v_l} \frac{d\rho_g}{d\rho} \frac{SF P_l}{SF G_r} = 0.1 \cdot \frac{1}{50 \cdot 0.5} \cdot \frac{2500}{20} = 0.5$$

$$P118 = 2 \cdot SF T_{t2} = 0.04$$

$$P114 = \frac{k_t}{T_t} \frac{SF T_{t2}}{SF(T_{t1} - T_{t2})} = \frac{22.5}{33} = 0.6818$$

$$P109 = \frac{1}{k_r} \frac{SF(T_{t2} - T_{ro})}{SF Q_r} = \frac{1}{11.4} \cdot \frac{250}{50} = 0.4386$$

$$P102 = \frac{1}{C_t} \frac{SF T_{t2}}{SF Q_r} = \frac{1}{33} \cdot \frac{250}{50} = 0.1515$$

$$P112 = \frac{1}{10} \cdot \frac{1}{v_l} \frac{1}{\rho_g C_p} \frac{SF T_{ro}}{SF Q_r} = 0.1 \cdot \frac{1}{50 \cdot 5 \cdot 0.0025} \cdot \frac{250}{50} = 0.8$$

$$P116 = 10 \cdot v_r \cdot g \cdot \frac{SF G_r \cdot SF(T_{ro} - T_{ri})}{SF T_{ro}} = 10 \cdot 50 \cdot 5 \cdot \frac{50}{2500 \cdot 100} = 0.5$$

$$P89 = \frac{1}{10} \cdot \frac{SF T_{ro}}{SF(T_{ro} - T_{ri})} = 0.1 \cdot \frac{100}{50} = 0.2$$

$$P50 = \frac{1}{10} \cdot (\text{zerop. } T_{ro} - \text{zerop. } T_{ri}) \cdot SF T_{ro} = 0.1 \cdot (250 - 175) \cdot \frac{1}{50} = 0.15$$

$$P119 = \frac{10}{h_{fg}} \frac{SF G_l}{SF Q_r} = \frac{10}{1.57} \cdot \frac{250}{2000} = 0.7962$$

IC-value potentiometers:

$$P75 : P_h$$

$$P70 : P_l$$

$$P100 : T_{t2} \quad \text{zeropoint: } 250^\circ\text{C}$$

$$P110 : T_{ro} \quad - \quad - \quad : 250^\circ\text{C}$$

DFG table

$$F77: Y_v(p_h/p_v)$$

$X = p_h/p_v$	$Y$
0.000	1.0000
0.575	1.0000
0.625	0.9943
0.675	0.9752
0.725	0.9414
0.775	0.8906
0.825	0.8191
0.875	0.7200
0.925	0.5787
0.950	0.4809
1.000	0.0000

APPENDIX E

Analog diagram and potentiometer list for the electrical power grid model.

Potentiometer list

$$P105 = \frac{1}{r_{a1}} \frac{SF(E_g - E_{gr})}{SF A_v} = \frac{1}{0.004} \cdot \frac{2}{1000} = 0.5$$

$$P97 = \frac{1}{r_{gr}} \frac{SF \Delta f / f_n}{SF \Delta E / E_n} = \frac{1}{7.5} \cdot \frac{50}{2.5} = 0.6667$$

$$P90 = \frac{1}{r} = \frac{1}{7.5} = 0.1333$$

$$P96 = \frac{100 \cdot E_2}{10 \cdot r_{2v}} \frac{1}{SF \Delta E_2 / E_2} = \frac{100 \cdot 0.1 \cdot 5}{10 \cdot 0.25 \cdot 50} = 0.4$$

$$P67 = \frac{SF \Delta E_2 / E_2}{SF \Delta f / f_n} = 1 \cdot \frac{5}{50} = 0.1$$

$$P94 = \frac{1}{10 \cdot r_{2v}} = \frac{1}{10 \cdot 0.25} = 0.4$$

$$P95 = P94 = 0.4$$

$$P107 = \frac{1}{10 \cdot r_{2t}} = \frac{1}{10 \cdot 0.5} = 0.2$$

$$P106 = \frac{E_2}{E_n} = \frac{4130}{5000} = 0.826$$

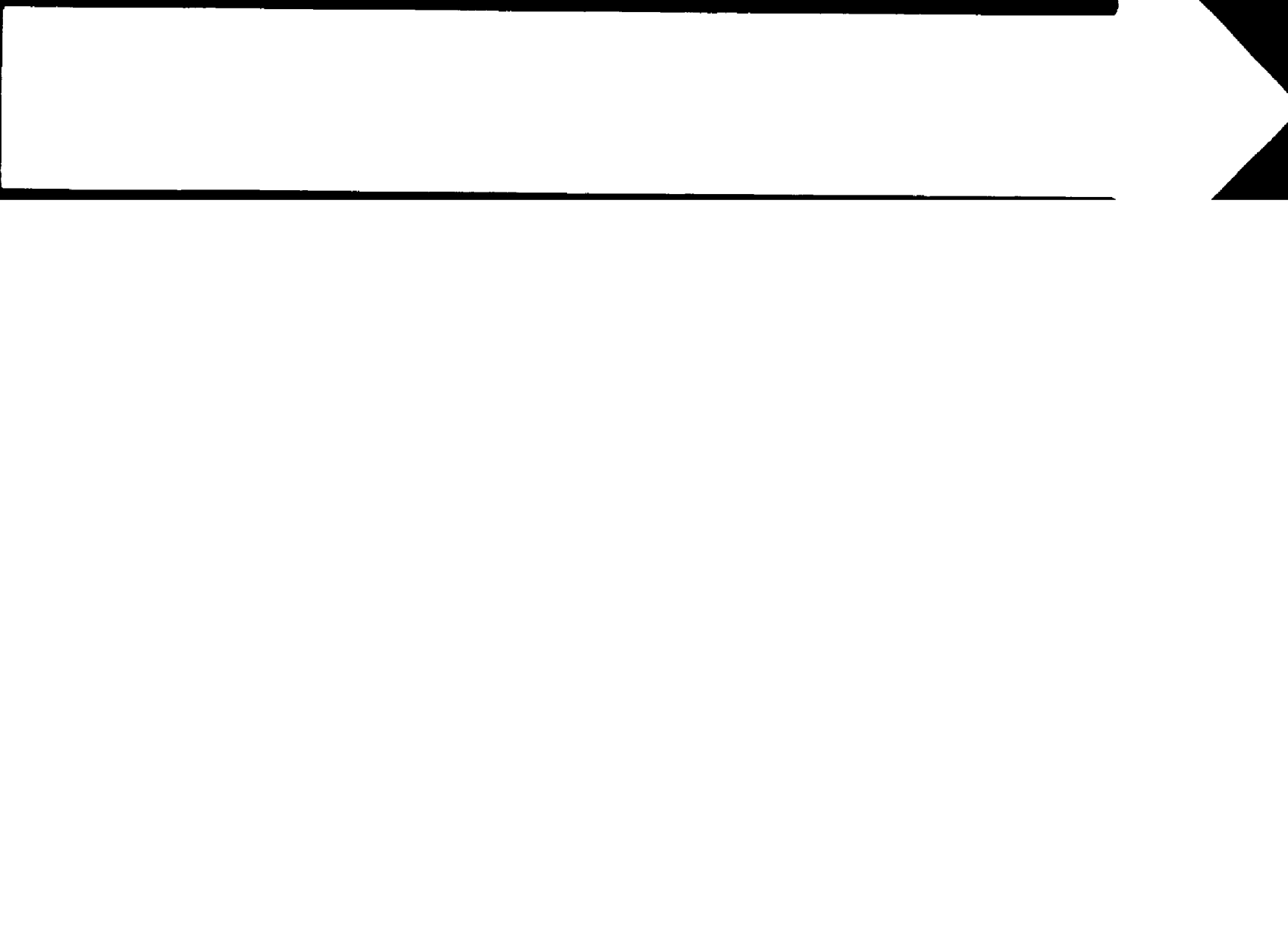
$$P108 = \frac{1}{E_n} \frac{SF \Delta E / E_n}{SF \Delta E_g} = \frac{1}{5000} \cdot 5 \cdot 1000 = 1$$

$$P68: 10\text{-value for } A_v/2$$

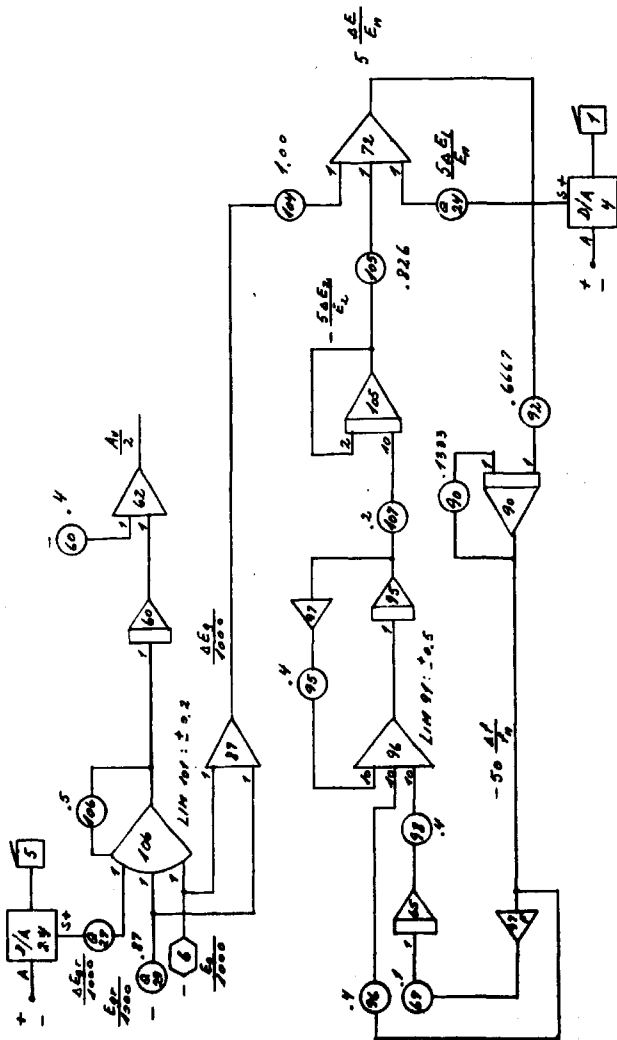
$$Q29: 5 \Delta E_1 / E_n$$

$$Q29: E_{gr}/1000$$

$$Q27: \Delta E_{gr}/1000$$






$$\text{MDAC} \quad 0: \quad \frac{N}{500}$$

-"- 1: (10 a)<sub>n</sub><sup>j</sup>

$$-n- \quad 2: \quad \frac{0.5759}{250 \text{ c}_{pp}}$$
$$-n- \quad 3: \quad \frac{0.580}{h_{fg}}$$
$$-n- \quad 4: \quad 10 \frac{\rho_{gs}}{\rho_{fs}}$$

-n- 5:  $0.8948(1-a_t)$

$$-''- \quad 6: \quad \frac{E_g}{1000}$$
$$-n- \quad 7: \quad - \frac{\Delta T}{100} \text{ ps}$$

-n- 8:  $\frac{\Sigma N}{5000}$

-n- 9:  $\frac{C_{bor}}{2000}$

$$-n- \quad 10: \quad \frac{V_f - 12}{20}$$

-7- 11:  $\frac{w_e}{50}$

- 12:  $\frac{W}{50}$

- 13:  $\frac{T_{P2}}{50}$

$$A_0 = \frac{\Delta P_D}{20}$$
$$-''- 1: -(\frac{\Delta T}{500}) \frac{1}{n}$$
$$-n-2: \left( \frac{\Delta T_{Ca}}{100} \right) \frac{1}{n}$$

Reactor

— 11 —

### Steam generator

- 9 -

- 11 -

**Turbine**

- 11 -

## Pressurizer

Reactor

- 9 -

### Pressurizer

— 11 —

**—H—**

### Steam generator

### Prespurizer

## Reactor

$$\begin{aligned} \text{AO } 3: & \left( \frac{\Delta T_c}{50} \right)_n^j \\ \text{"- } 4: & \frac{T_{pi}}{50} \\ \text{"- } 5: & \left( \frac{\sum Q_k}{500} \right)_n^j \text{ or } \frac{\Delta T_{Ga}}{50} \\ \text{"- } 6: & - \frac{T_{p1}}{50} \\ \text{"- } 7: & \frac{T_{p12}}{50} \end{aligned}$$

$$\begin{aligned} \text{AI } 0: & \left( \frac{Q_k}{50} \right)_n^j \\ \text{"- } 1: & - \left( \frac{\Delta T_u}{25} \right)_{n+1}^j \\ \text{"- } 2: & \left( \frac{\Delta T_{ca}}{25} \right)_{n+1}^j \\ \text{"- } 3: & \left( \frac{\Delta T_c}{10} \right)_{n+1}^j \\ \text{"- } 4: & (100 \Delta T_a)_{n+1}^j \\ \text{"- } 5: & - \frac{\rho_m - 500}{500} \\ \text{"- } 6: & \frac{W_i}{15000} \\ \text{"- } 7: & \text{CR-position} \end{aligned}$$

$$\begin{aligned} \text{"- } 8: & W_b \\ \text{"- } 9: & \text{Not used} \end{aligned}$$

$$\text{"- } 10: - \frac{T_{p0}}{50}$$

$$\text{"- } 11: \text{Not used}$$

$$\text{"- } 12: \frac{\Delta P_s}{75}$$

Reactor

Turbine

Reactor

Steam generator

- " -

Reactor

-"

-"

-"

-"

-"

-"

-"

Primary loop

Steam generator

Steam generator

$$\text{AI } 13: \frac{T_{ss}}{50}$$

Steam generator

$$\text{"- } 14: \frac{W_p}{5000}$$

- " -

$$\text{"- } 15: \text{Not used}$$

$$\text{"- } 16: \frac{P_h}{100}$$

Turbine

$$\text{"- } 17: \frac{P_1}{70}$$

-"

$$\text{"- } 18: \frac{Q_r}{250}$$

-"

Error messages:

System errors: FFP DIV. Ø  
FFP EXP. OVERFLOW

Both messages are self-explanatory. No exit address is given, but it may be found by ODT in APT(9-11) plus (APT+1). The octal address for APT is given in the address list in appendix A.

FILE ERR.

FILE END

occurs only in connection with reading from disk files, an IC file or a static data file. The first means that the file is not present on the disc, the other means that the file is too short.

Program errors:

NEG.WC :  $W_c$  goes negative  
NEG.WP :  $W_p$  goes negative  
STANG POS. NEG. : Regulating rod position goes negative  
DIV.OVERFL.BOR : Overflow by division during calculation of boron acid concentration  
C-BOR NEG. : Boron acid concentration goes negative  
FOR LANG REGNETID : The calculation for one time step takes more than 0.1 sec., possibly due to a long "track" time in the core hybrid computations (MM Ø)

TRAP6 messages:

0-7: Overflow by conversion of nuclear power to integers for core sections 3-10.

Section power > 500 MW.

20	Overflow T-lower plenum	$ T-300  > 50^\circ C$	MDAC 0
21	- " - $T_{pl}$	- " -	A0 6
22	- " - $T_{pl2}$	- " -	A0 7
24	- " - $0.5759/(250 c_{pp})$		MDAC 2
25	- " - $0.580/h_{fg}$		MDAC 3
26	- " - $10 \rho_{gs}/\rho_{fs}$		MDAC 4
30	- " - $0.8948 (1-a_t)$		MDAC 5
31	- " - $E_g/1000$		MDAC 6
32	- " - $T_{ri}$	$ T-175  > 50^\circ C$	A0 4
40	- " - $p_p$	$ p-150  > 20 \text{ bar}$	A0 0
41	- " - $v_f$	$ v_f-22  > 10 \text{ m}^3$	MDAC 10
42	- " - $W_e/50$		MDAC 11
43	- " - $W_c/50$		MDAC 12
44	- " - $T_{ps}$	$ T-350  > 50^\circ C$	MDAC 7

Limiter settings:

LIM 31 = ±1 saturation limiter for  $\Delta T_{ca}$   
" 51 = ±1 - " - " - "-  
" 71 = 0, +1 exact  $0 \leq (T_{ps} - T_c)/50 \leq 1$   
" 91 = ±0.5  $(SF \Delta E_2/E_2)/T_{v2} = 5/10$   
" 101 = ±0.2  $(SF A_v/2)/T_{v1} = 0.5/2.5$

MM pulse length:

MM 00 = 100 µs  
MM 01 = 100 "  
MM 02 = 100 "  
MM 40 = 100 "





[illegible]

```

POP.      STARTF
          SETX INX
          BRSE DT
          SETB DT
          /BEREIGNING
          DPOL:ROFS,KRFS,2,P
          DPOL:ROGS,KRGS,2,P
          DPOL:RVSF,KVSF,2,P
          DPOL:RQSF,KRQSF,2,P
          DPOL:RFS,KVFS,2,P
          DPOL:RHS,KHGS,2,P
          DPOL:RHSF,KHVSF,2,P
          DPOL:RHSF,KHVSF,2,P
          DPOL:RPH,KAPH,2,HF
          DPOL:RPH,KRPH,1,HF
          DPOL:RQP,KRQP,1,HF
          DCAL:HF=SF+RPH+ROFS*RF
          DCAL:HF=HSG+RHS+ROGS*RG
          DCAL:HS=HFS*HF
          DCAL:HG=HGS*CPH:KS:P=P-DTSP-DTV*XS:DTQV
          DCAL:K=QGV:QGV/CI*TVF
          /BEREIGNING AB NY TILSTAND
          STARTF
          FLDA FRI:JED FUNS
          /VMMH
          DCAL:PP=RVSP+VF=-MI+MC=NE/ROFS:VFP
          JA Q3
          /VMMH
          DCAL:HF=RF*XI:XS:PP=RP+P*XS+VF=-MI+MC/RF:VFP
          FLDA BAI:JED GUN1
          /DAMP HAEITET
          DCAL:PP=RVSP+VF=HE+HC=NR/VQ:ROSP:PP
          JA FR2
          /DAMP UHAETET
          DCAL:VBN=HPR:INIS
          EQVVF+P*MC=MC=NR*XS:VQ/RGP:VP
          /NE,MC,PP,HG,BEREIGNING
          FLDA MI:JGT +3,FCLA:FSTA NIP
          FLDA FRI:JED GUN2
          /VMMH
          DCAL:ROFS=HVSF-FBS:PP+VF:XI
          DCAL:MI=-HVS:MI+P*XS:XI:WFD+HSE/F2
          JGT +3,FCLA:FSTA MC:FSTA FRI
          JA Q3
          /DAMP UHAETET
          DCAL:HF=MI+HVS:FXS:HE=HF+MC=XS:XI
          DCAL:PP=VF+P*XS:XS:VF=HF+P
          FLDA BAI:JED GUN2
          /DAMP HAEITET
          DCAL:ROGS=HVSF-FBS:PP+VF:XI
          DCAL:RHS=HMK=MC*XI:QGV/HFG
          JGT +3,FCLA:FSTA MC:FSTA GRI
          JA Q3
          /DAMP UHAETET
          DCAL:HF=HMK=MC*XS:HS=HF+MC=XS:XI
          DCAL:PP=VF+P*XS:XS:QGV/VF+HFG
          STARTD
          FLDA INX1+2
          JED FRI
          STARTF
          FLDA FRI:JNE MID1
          DCAL:HFP=D*HF+HF
          FSUB HFS,LYL DMO
          DCAL:HVS,HP,FRI
          MID2
          FLDA GRI:JNE MID2

```

```

MID2  OVAL HQP*DT*MG*MG
      FSLD HQS:JGT DPOV
      OVAL HQS:MG*GMI
      /UDREGM DELTA P DG VF
      OVAL PP*DT*P
      OVAL VFP*DT*VF
      OVAL V-VF*VG
      OVAL TWP*DT*DTV
REC.  /BEREGM REGULERINGIS INPUT VARIABLE
      OVAL PB-P-QD
      JGT +2.FCLA
      OVAL +MK+QD*Q
      FSLD ON:JLE +4.FLDA' ON:FSTA' Q
      OVAL P-PB-MKD
      JGT +3.FCLA
      OVAL +MK+MKD*MK
      FSLD MKN:JLE +4.FLDA' MKN:FSTA' MK
      OVAL P-PB-MKD
      JGT +5.FCLA JR +3.FLDA' MKN:FSTA' MK
      FLDA MIST:JGT MIRA
      FLDA TT:JLE FLUD
      FSLD DT:FSTA TT:JGT FLUD
      FLDA MIRA:FSTA MI
      FLDA TT:JGT MIRA1
      FLDA MIRA1:JNE FLUD
      FLDA DMI:FSTA DMI
      FLDA DMI:FSTA TT
      FLDA F1:FSTA MIRA'
      FLDA TT
      FSLD DT:FSTA TT
      FLDA DMI:FSTA MI
      JSR UOL
      STARTD
      FLDA D1
      FNEB
      PADDNB INCL*2
      JR FOP
      /
      /VALUES VARIABLE
      JR 0
      OPIX:0.P.PB.SP.DVNO
      OPIX:1.VF.VFV.SVF.OVA1
      OPIX:2.ME..SME.OVA2
      OPIX:3.MC..SME.OVA3
      OPIX:4.MC..SME.OVA4
      OPIX:5.MC..SME.OVA5
      OPIX:6.B..SB.OVA6
      OPIX:7.PP..SPP.OVA7
      /
      SETX INCL
      FLDA FMI /INCL(0)=1 FOR VAND HRETHING
      JGT +0
      FLDA' F1
      JR +3
      FCLA
      DTG 0
      FLDA DMI /INCL(1)=1 FOR DAMP HRETHING
      JGT +0
      FLDA' F1
      JR +3
      FCLA
      SETX 1
      JSR UOL

```

```

OVA2. TRAP6 2
OVA3. TRAP6 3
OVA4. TRAP6 4
OVA5. TRAP6 5
OVA6. TRAP6 6
OVA7. TRAP6 7

```

- 104 -

- 105 -

# APPENDIX J

Program listing for the detailed steam generator model, a set of IC-values and an input-output example.





16-values according to statement 100

[illegible]

108 -

607 -



# APPENDIX K

List of files on DEC-tape "PNR DEC.74"

TAPE: PWR DEC. 1974

FPL.FP: FLAP LIBRARY FILE, DEC'S SYSTEM  
SL.FP: FLAP LIBRARY FILE, HYBAL SYSTEM  
HSL.FP: FLAP SYMBOL TABLE EXTENSION  
ML.ML: 8BAL LIBRARY FILE, HYBAL SYSTEM

P1.FT: TEN-SHELL SECTION FUEL MODEL  
P1.LD: DO IN LOAD FORMAT  
P3.FT: STEAM GENERATOR MODEL  
P3.LD: DO IN LOAD FORMAT  
P3100.IC: IC-FILE FOR DO, 100% LOAD

P2.8B: PRESSURISER MODEL  
P2.SV: DO IN SAVE FORMAT

PWR.8B: PWR PLANT MODEL, PDP8 CODE SECTION  
PWR1.8B: DO , FPP CODE SECTION 1  
PWR2.8B: DO , DO DO DO 2  
PWR3.8B: DO , DO DO DO 3  
PWR.SV: DO IN SAVE FORMAT  
PWR.IC: IC-FILE FOR DO  
PWR.ST: STATIK DATA FOR DO  
PWR.SP: POTENTIOMETER FILE FOR DO

12/16/74  
LABEL 2 12/16/74  
FPL.FP 58 6/14/73  
SL.FP 26 10/29/74  
HSL.FP 2 2/12/74  
ML.ML 31 11/15/74  
P1.FT 7 12/10/74  
P1.LD 15 12/10/74  
P3.FT 17 12/10/74  
P3.LD 19 12/10/74  
P3100.IC 8 12/10/74  
P2.8B 18 12/4/74  
P2.SV 14 12/4/74  
PWR.8B 33 12/14/74  
PWR1.8B 16 12/6/74  
PWR2.8B 26 12/11/74  
PWR3.8B 20 11/25/74  
PWR.SV 37 12/11/74  
PWR.IC 3 12/16/74  
PWR.ST 30 12/16/74  
PWR.SP 5 12/11/74  
(EMPTY) 343  
343 FREE BLOCKS

# APPENDIX L

Example of logging of main variables for the power plant model.

FLUX:

1.507 E+013					
2.862 E+014	3.313 E+014	3.881 E+014	3.970 E+014	3.888 E+014	
3.592 E+014	3.491 E+014	3.397 E+014	3.506 E+014	3.609 E+014	
3.487 E+014	3.150 E+014	2.595 E+014	1.815 E+014		
1.416 E+013					

NUKLEAR EFFEKT I MW:

120.3	192.7	224.8	228.8	218.4	204.9	198.8
192.2	198.2	203.9	195.9	175.9	144.1	100.3

URAN TEMP.:

474.5	611.0	679.3	692.3	675.2	651.3	642.5
632.5	648.6	663.5	650.5	614.2	556.3	479.4

KAPSEL TEMP.:

295.9	306.4	313.1	317.8	319.1	320.8	323.8
325.1	328.5	331.9	333.7	334.8	332.5	329.2

VAND TEMP.:

281.7						
283.5	286.5	289.9	293.3	296.6	299.5	302.4
305.2	307.9	310.7	313.3	315.6	317.5	318.8
318.9						

VAND TÆTHED:

.7602						
.7604	.7558	.7492	.7424	.7358	.7294	.7236
.7175	.7114	.7053	.6987	.6921	.6865	.6823
.6838						

VOID I X:

.00	.01	.02	.03	.05	.06	.00
.11	.15	.20	.27	.36	.44	.52

FASTE KONTROLSTÆNGER:

.000						
.000	.100	.200	.300	.400	.500	.600
.200	.150	.000	.000	.000	.000	.000
.000						

REAKTOR EFFEKT : 2597.6  
REG. STANG POS. : .5112  
REG. STANG VÆGT : .2000  
BOR KONCENTRATION I PPM: 1440.7  
PRIMER TRYK: 140.64  
PRIMER RØTNINGSTEM: 245.28  
DAMPTRYK : 80.00  
DAMPTEMP.: 200.00  
DAMP DELASTID I KG/MM<sup>2</sup>:  
HP YUNDING TRYK: 80.00  
LP YUNDING TRYK: 14.00  
EL EFFEKT I MW: 2597.6